Flow Modeling and Testing of ESPs

ICESP 2018 Charlotte, NC, USA

Robert Mudry, P.E.
Airflow Sciences Corporation
Livonia, MI, USA
rmudry@airflowsciences.com

Outline

- Introduction
- ESP Fluid Flow Basics
- Flow Modeling
 - Physical scale
 - CFD
- Questions



ESP Fluid Flow Basics

Primary goal: Maximize particulate capture

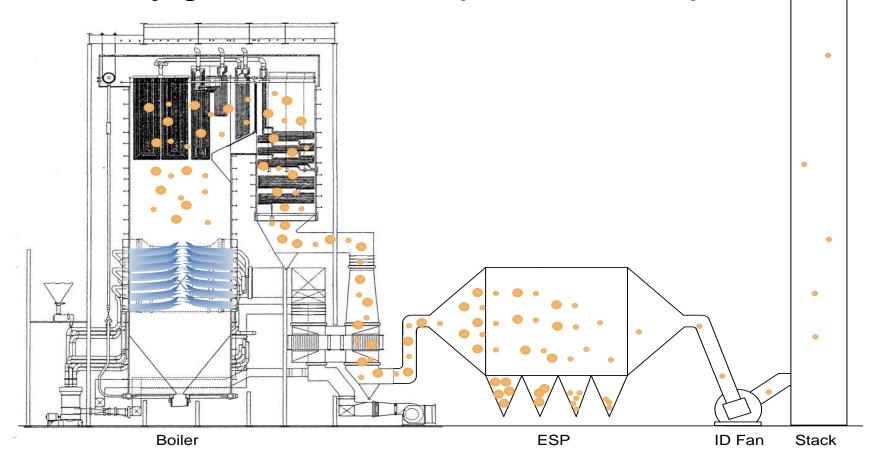


Image: Gerry Klemm, Southern Company



ESP Fluid Flow Basics

Flow Related Goals

- Uniform gas velocity through collection fields
- Equal flow balance between multiple chambers
- Avoid hopper re-entrainment
- Avoid particulate deposition / drop out
- Minimize peak velocities / erosion
- Minimize pressure drop
- Uniform temperature distribution
- Sorbent injection / mixing



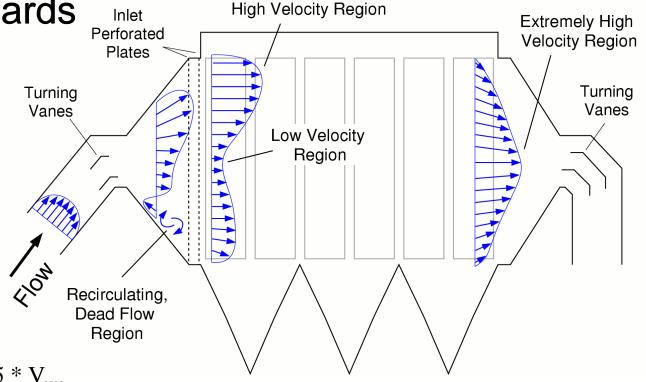
Gas Velocity Distribution

Uniform velocity within collection region

Industry standards

• ICAC

RMS/CV deviation



ICAC: 85% of velocities $\leq 1.15 * V_{avg}$

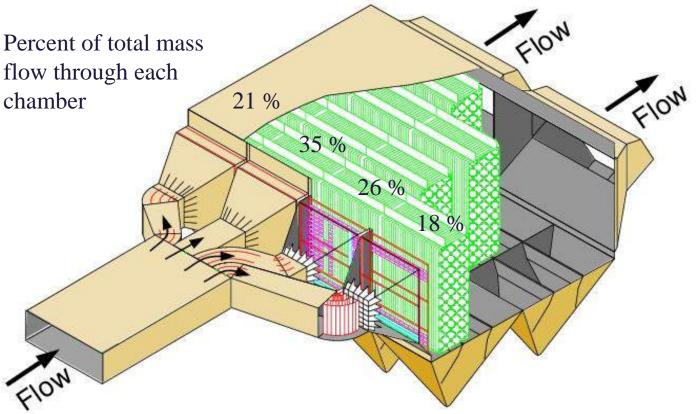
99% of velocities $\leq 1.40 * V_{avg}$

Other: % RMS Deviation $\leq 15\%$ of V_{avg}



Gas Flow Balance

❖ ICAC goal: flow within ±10% per chamber

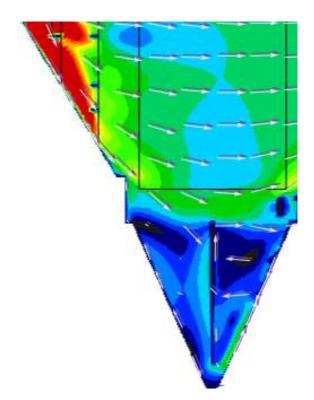


ICAC: Flow within each chamber to be within $\pm 10\%$ of its theoretical share

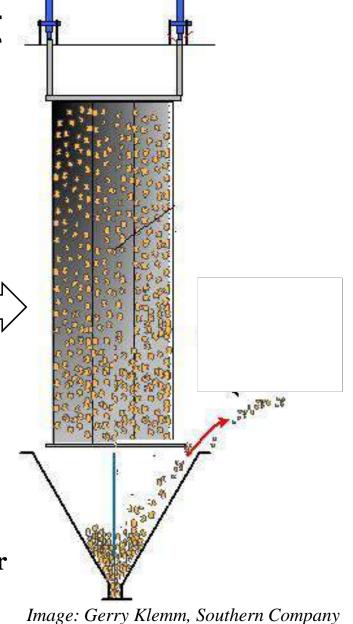


Hopper Re-entrainment

- Avoid gas flow in hoppers
- Avoid sweepage



Particles escape due to gas flow in hopper





Particulate Deposition

- Duct floors
- Turning vanes
- Perforated plates



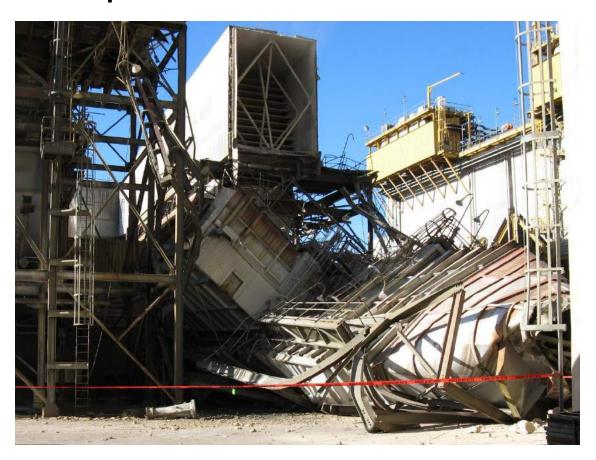




Particulate Deposition

❖ Extreme deposition

■ structural failure



Peak Velocities / Erosion

Erosion potential depends on

- Impact velocity (to the 2.5 power)
- Flow rate
- Hardness, shape
- Angle of impact

Erosion issues

- Vanes
- Baffles
- Perforated plates
- Ductwork
- Trusses

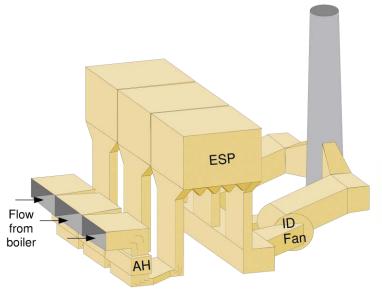


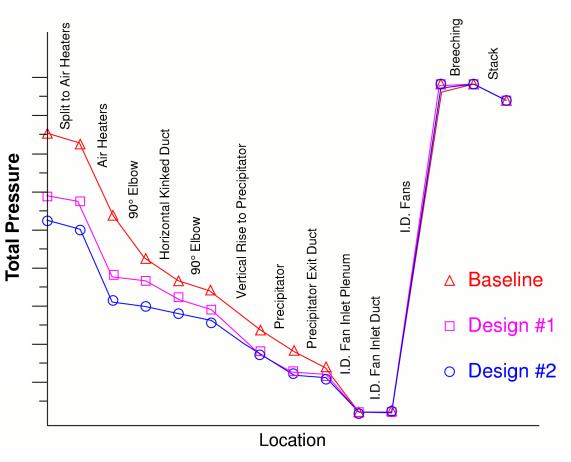




Pressure Drop

- General goal:
 - Minimize DP



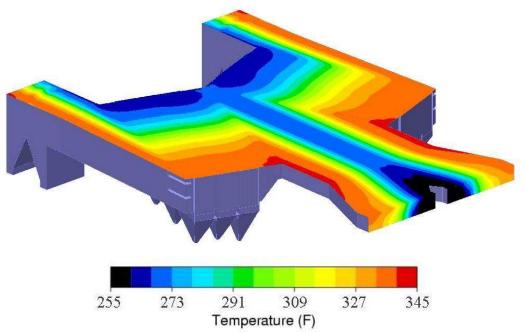


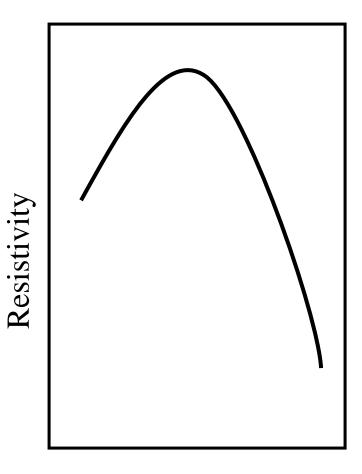
Ductwork redesign saves 2.1 IWC (520Pa)



Gas Temperature

- Temperature stratification
 - Resistivity
 - Corrosion
 - Sorbent performance



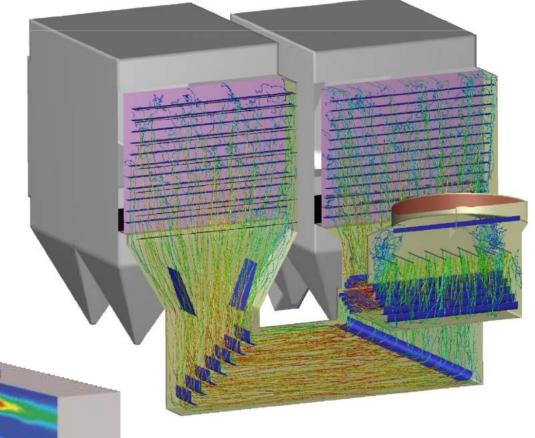


Temperature



Injection Systems

- Gaseous injection
 - SO3, NH3, others
- Particulate injection
 - Activated carbon
 - Trona, SBS, lime, etc.

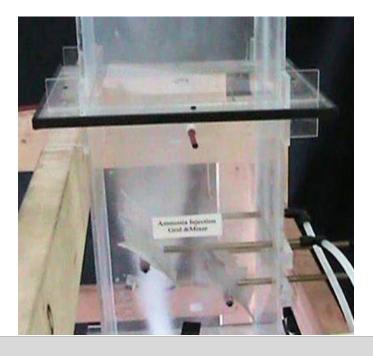


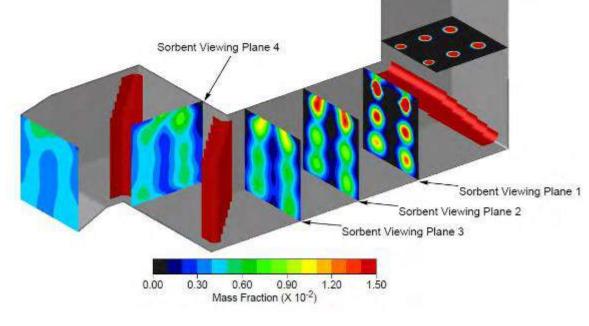


Sorbent Injection

Goals

- Uniform distribution
- Surface contact / residence time
- Mixing / dispersion

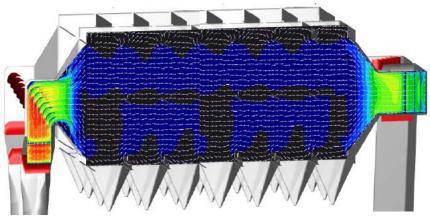




ESP Modeling

- Physical Model Testing
- Computational Fluid Dynamics (CFD)





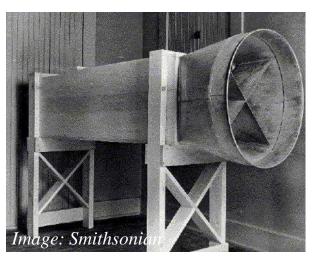
ESP Modeling – Physical Models

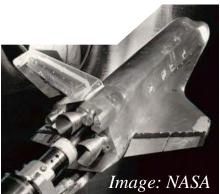
- Background
- Theory
- Simulation Parameters
- Fabrication Details
- Results Analysis
- Flow Visualization



Physical Models – Background

- Utilized for fluid flow analysis for a century ... or more?
- Applied to ESPs for decades
- Underlying principle is to reproduce fluid flow behavior in a controlled, laboratory environment







Physical Models – Theory

- Key criteria is to generate "Similarity" between the scale model and the real-world object
 - Geometric similarity
 - Accurate scale representation of geometry
 - > Inclusion of all influencing geometry elements
 - > Selection of scale can be important
 - Fluid dynamic similarity
 - > Precise Reynolds Number (Re) matching is not feasible
 - General practice is to match full scale velocity but ensure that Re remains in the turbulent range throughout the model

$$Re = \frac{\rho \ v \ D_h}{\mu}$$



Physical Models – Parameters

ESP geometry

- Typically 1/8th to 1/16th scale
- Include features affecting flow patterns

Flow conditions

- Scaled air flow rate (at ambient temperature)
- Simulate injections with a tracer gas
- Simulated particle tracking
 - > In flight
 - > Deposition



Physical Models – Fabrication Details

More detail is better

- Vanes, splitters, baffles
- Trusses, gusset plates
- Dampers, columns





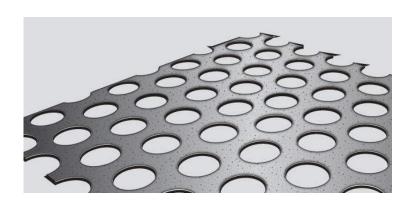


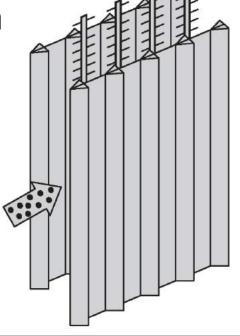
Physical Models – Fabrication Details

- Perforated plate selection
- Collection plate representation

Geometry / loss coefficient

Re consideration







Physical Models – Results Analysis

Quantitative data

- Available at discrete measurement points
- Velocity magnitude, directionality
- Pressure (corrected to full scale)
- Tracer gas concentration
- Mass balance between chambers
- Comparison to ICAC conditions
- Correlation to test data

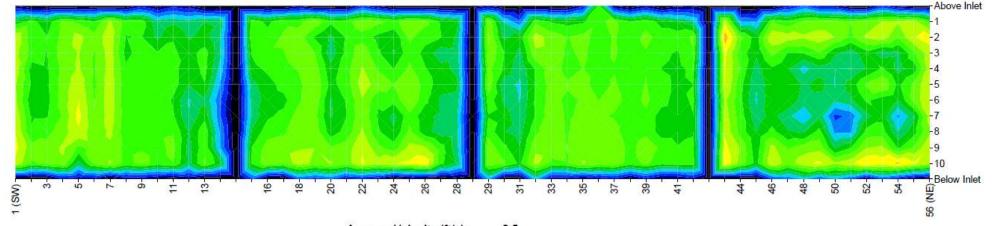
Qualitative data

- Flow directionality (smoke, tufts)
- "Dust Test" for particle behavior, drop-out, re-entrainment



Physical Models – Velocity Results

Uniformity vs. ICAC goals



Average Velocity (ft/s): 8.5

%RMS Uniformity: 12.1% (Target: <15%)
% of points <115% of average: 90.7% (Target: >85%)
% of points <140% of average: 100.0% (Target: >99%)

% of lower 25% of area >71% of average: 100.0% (Target: >99%)





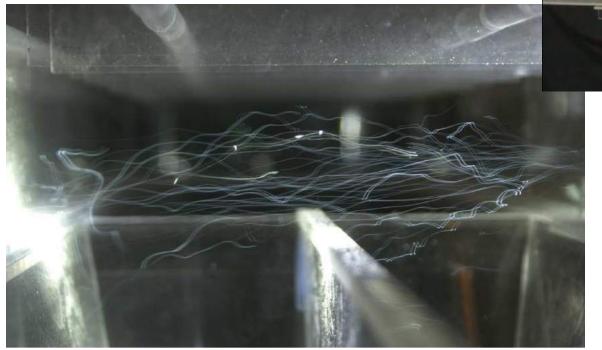
Physical Models – Dust Testing





Physical Models – Visualization

- Smoke flow
- Helium bubbles





Images: Gerry Klemm, Southern Company



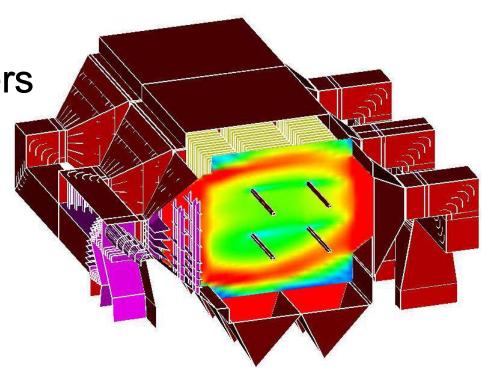
Physical Models – Visualization

Video footage



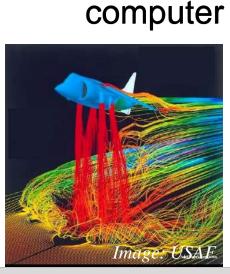
ESP Modeling – CFD

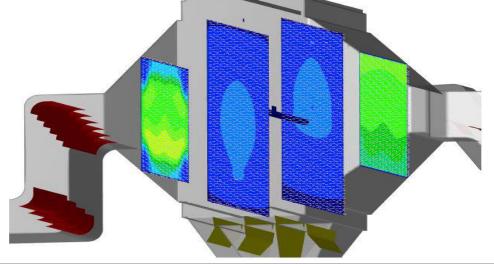
- Background
- Theory
- Simulation Parameters
- Mesh Details
- Results Analysis
- Flow Visualization

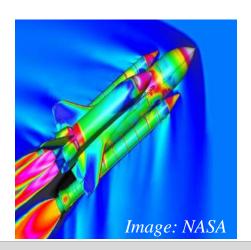


CFD – Background

- Developed in the aerospace industry c.1970 (with the advent of "high speed" computers)
- Applied to ESPs for 30+ years
- Underlying principle is to solve the first-principles equations governing fluid flow behavior using a

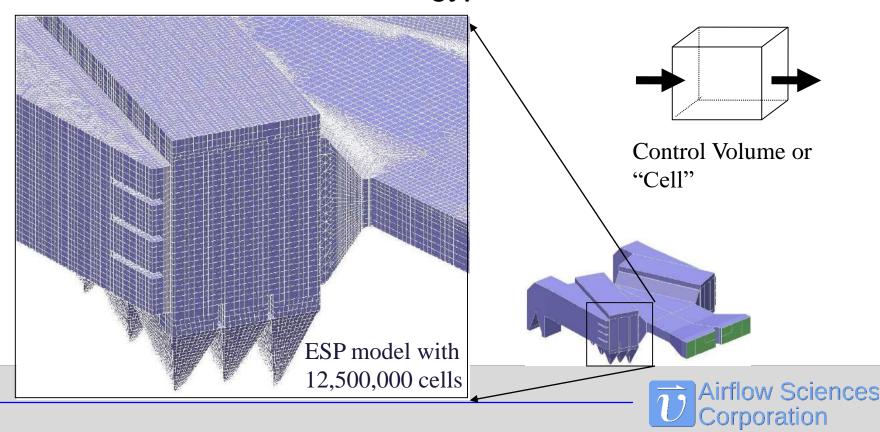






CFD – Theory

- Control Volume Approach
 - Divide the flow domain into distinct control volumes
 - Solve the Navier-Stokes equations (Conservation of Mass, Momentum, Energy) in each control volume

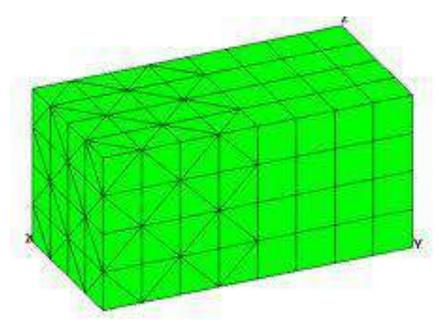


CFD – Mesh Details

- A good mesh is critical for accurate results
 - Cell count
 - Length scale
 - Local refinement
 - Shape/topology
 - > Hex vs. Tet vs. Poly
 - Flow alignment

❖ Why?

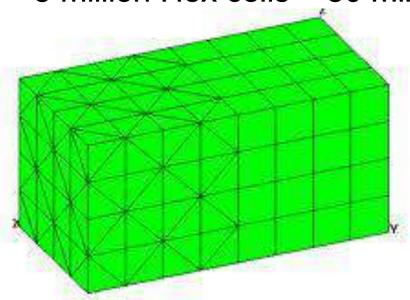
- Numerical calculation scheme accuracy is influenced by cell topology

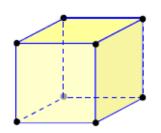


CFD Mesh Quality – Cell Topology

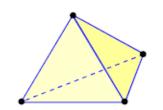
- Not all CFD cells are created equal
 - Hexahedral vs. Tetrahedral vs. Polyhedral
 - Tet mesh ≡ easier, automeshing
 - Hex or hybrid mesh

 harder, hand built
 - 5 million Hex cells ≡ 30 million Tet cells





Hexahedral cell (6 faces)



Tetrahedral cell (4 faces)

6 Tet cells fit into 1 Hex cell of the same length scale



CFD – Mesh Details

Direct geometry inclusion

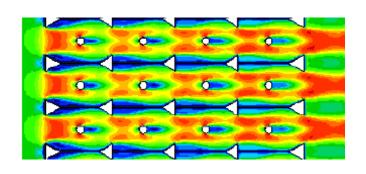
Vanes, baffles

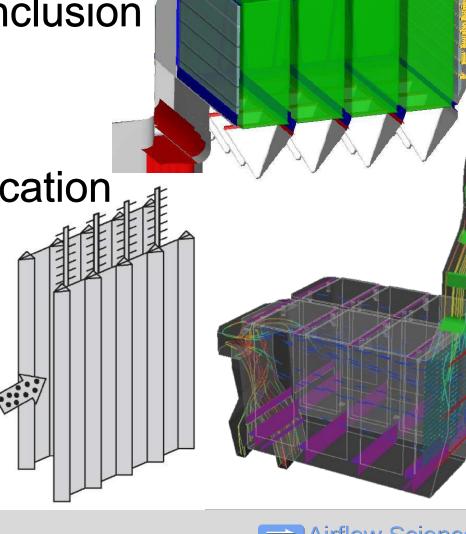
Structure

Numerical simplification

Perforated plates

Collection plates





CFD – Simulation Parameters

ESP geometry (mesh)

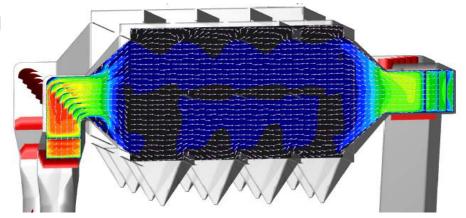
- > Full scale representation
- > Include features important to flow, more detail if possible

Flow conditions

- > Full scale gas flow rate
- > Reproduce velocity & temperature profile at model inlet
- Simulated chemical injection
- > Simulated particle tracking

Solver

- > Azore
- > Fluent
- > Star CCM+





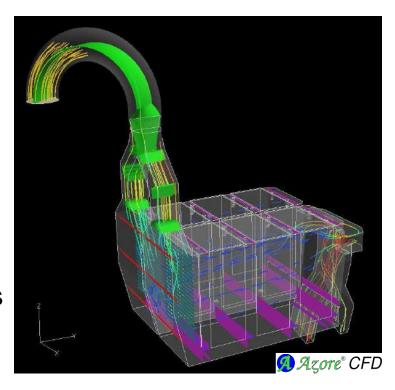
CFD – Results Analysis

Quantitative data available at all control volumes

- > Velocity magnitude, directionality
- > Temperature
- > Pressure
- > Turbulence
- > Chemical species concentrations
- > Particle trajectories

Integrated/reduced data

- Mass balance between chambers
- Comparison to ICAC conditions
- Correlation to test data



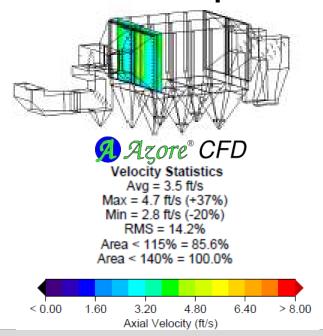
CFD – Results

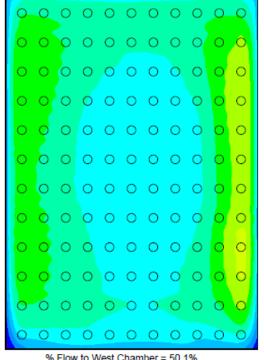
Velocity patterns

Uniformity vs. ICAC goals

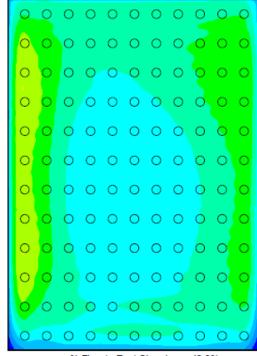
All cells vs. traverse

Pressure drop









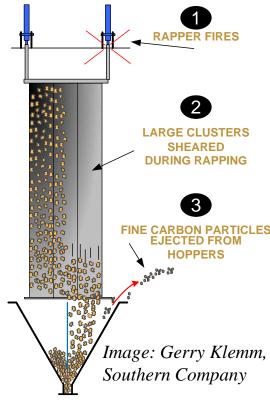
Total Pressure

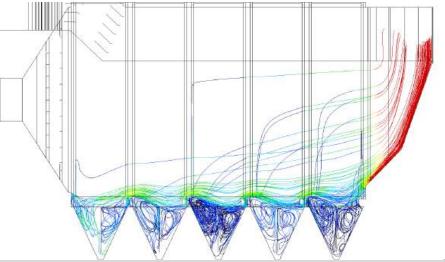
% Flow to East Chamber = 49.9%



CFD – Advanced Modeling

- Electrostatics
- Transient phenomenon
- Large meshes and HPC solvers
- Pressure pulses during to rapping
 - Hopper "splash"
 - Minimizing re-entrainment
- Chemistry / absorption





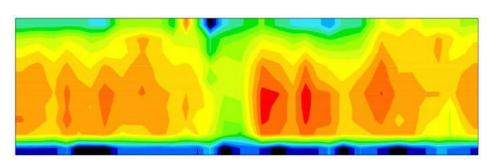
CFD – Flow Animations

Video footage



Model Correlation — Field Testing

- Velocity Distribution in ESP
 - Cold flow conditions
 - Vane anemometer
 - > Rides on plates / electrodes
 - Accuracy 1% in 3-10 ft/sec range
 - > Lightweight, portable
 - Sensitive to flow angularity, turbulence, dust
 - Difficult, expensive test





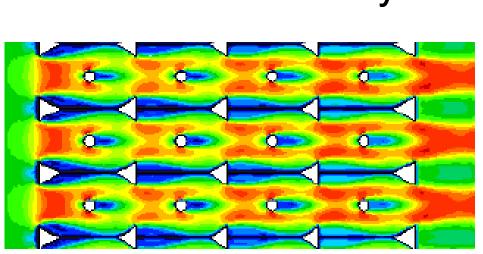




Field Testing – Collection Region

- Accuracy can be influenced by
 - Proximity to perforated plate
 - Collection plate geometry
 - Electrode geometry

Scrutinize the test data closely







Flow Model Accuracy

- Do physical and CFD models provide useful results, suitable for ESP design?
 - Yes, experience has shown that modeling is a dependable engineering tool
 - Useful for new ESPs and improving existing ESPs
 - Needs to be performed correctly and to the best of current modeling practices

Flow Model Accuracy

- Do the model results match actual plant data?
 - Not as well as one would like in some cases
 - Error bars are larger than desired
 - Correlation can be dependent on ESP geometry
 - Nozzle style inlets are particularly challenging for models
 - > Square and ladder vane style inlets have stronger correlation
- What to do when they don't match?
 - Re-evaluate the modeling, improve the methods
 - Scrutinize the test data



Flow Model Accuracy

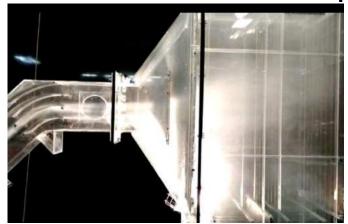
- Do CFD and physical models match each other?
 - Sometimes but not all
 - Correlation of uniformity statistics vs. profile
 - Limitations of both methods hamper correlation
 - Can be dependent on ESP geometry
 - > Inlet style nozzle vs. square
 - Flow devices and complexity
 - Research is ongoing
 - Speaker's experience in this area focuses on
 - 1. Perforated plate representation
 - 2. Collection plate representation

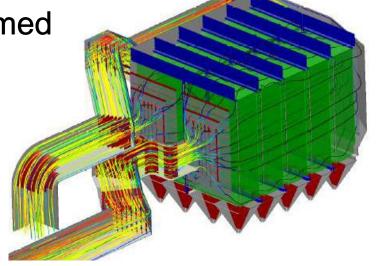


Summary – Industry Experience

- Hundreds of successful projects industry wide
 - Performance guarantees met
 - Reduced emissions / DP / maintenance

Field verification not often performed





Improved modeling methods would allow for additional ESP performance optimization



Summary – Key Takeaways

- Both CFD and physical modeling have been widely used for decades
- From a general view, the modeling methods provide beneficial engineering tools for design
- Both methods have specific procedures, and need to be done correctly to yield usable results
- Both methods have their limitations, their supporters, and their critics
- Research is ongoing on both methods, striving to improve accuracy and correlation

Acknowledements

- Dan Fahrer, DTE Energy
- Gerry Klemm, Southern Company
- Dr. Jia Mi, Southern Company
- Jose Sanchez, EPRI

Questions?



Contact Information



12190 Hubbard Street Livonia, MI 48510-1737 USA Tel. +1.734.525.0300

Robert G. Mudry, P.E.
President
rmudry@airflowsciences.com

www.AirflowSciences.com www.AzoreCFD.com www.AirflowSciencesEquipment.com

