

Analysis of Food Processing Operations Using a Coupled CFD/Food Model

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Motivation

Methods are needed for improving production scale food processing operations

Current tools:

- Research-scale testing**
- Pilot-scale testing**
- In-plant testing**
- Computer simulation**



Motivation

An effective simulation must include:

- . Prediction of the actual flow field**
- . Prediction of gas properties (T, RH)**
- . Effects of product on flow field**
- . Effects of local environment on product**
- . Effects of upstream product on environment**
- . Effects of product history**
- . Effects of product internal gradients**

Motivation

Why computational fluid dynamics (CFD) alone won't do:

Length scale problem

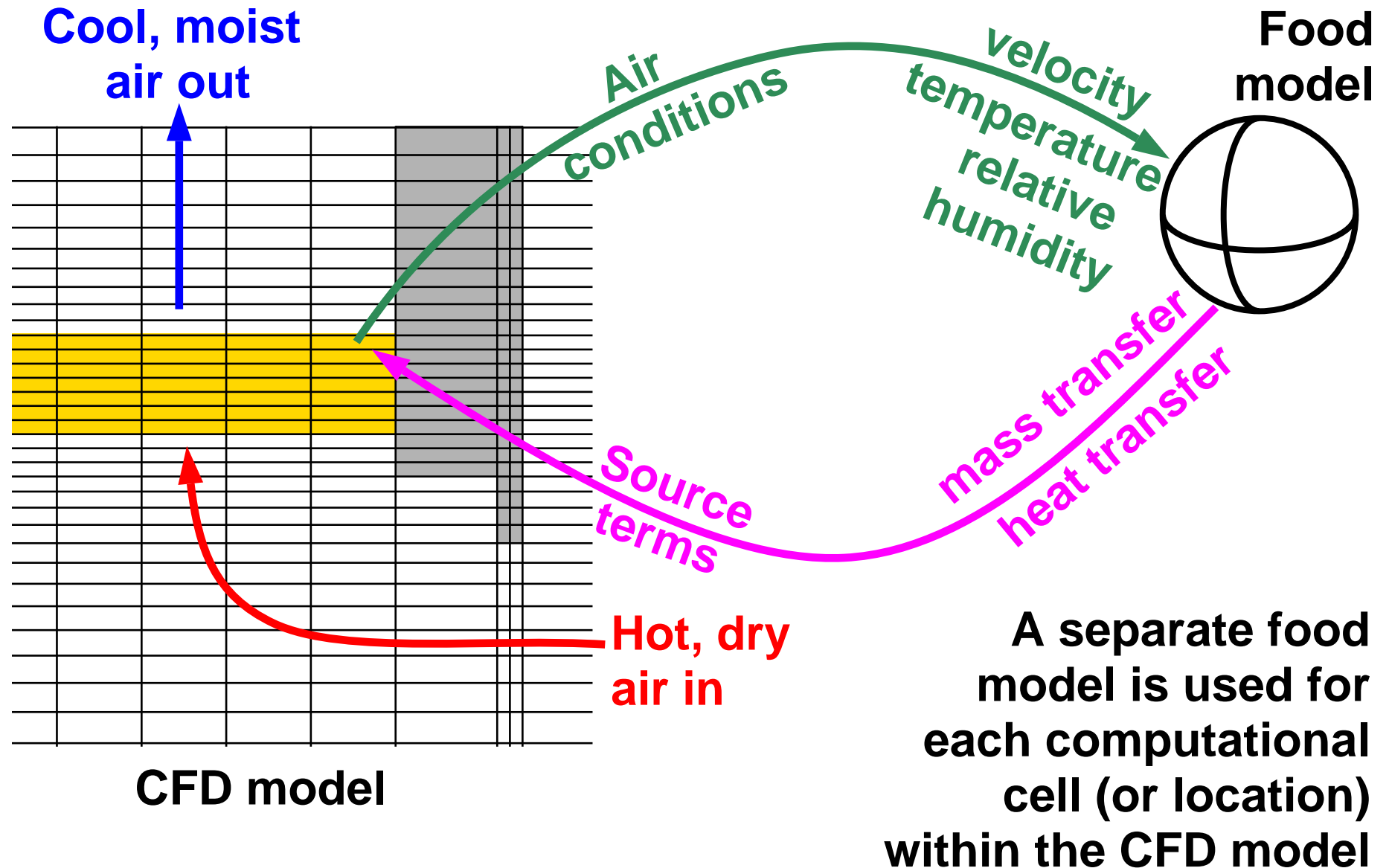
- . Food pieces much smaller than equipment**
- . Difficult to have sufficient grid density**

Movement problem

- . Belt motion**
- . Drop to lower level**
- . Continuously mixed**

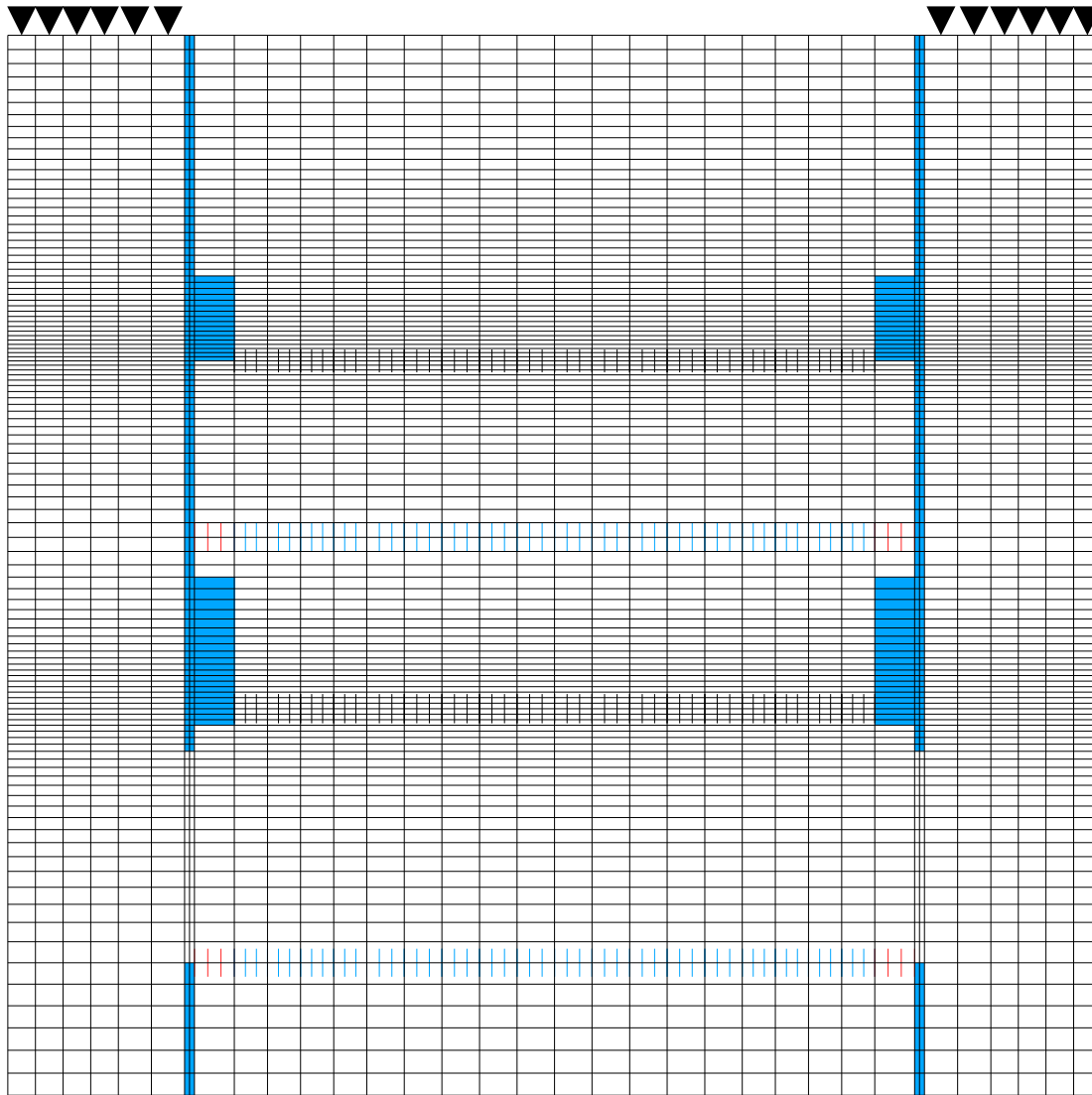
Approach

Couple CFD model of equipment to food models



Approach - CFD model details

Model domain divided into computational cells



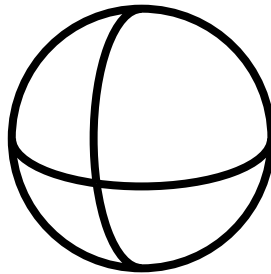
Differential equations solved across each cell for:

- momentum
- energy
- moisture
- pressure
- turbulence

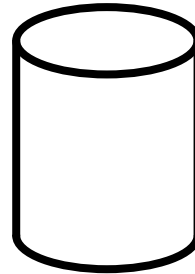
Approach - Food model details

1-D model for food internal gradients

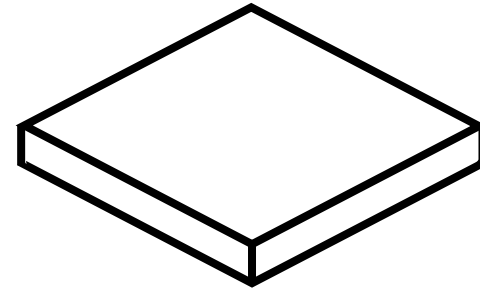
3 geometries



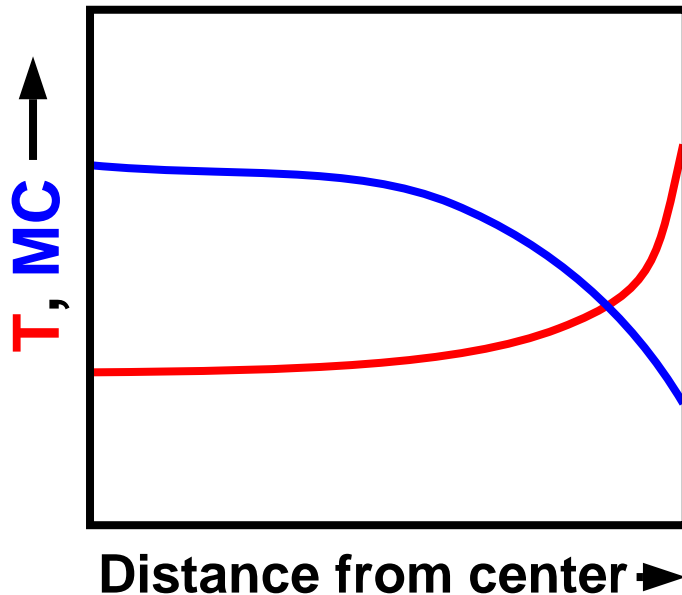
Spherical



Cylindrical



Plate



Fick's Law

$$D = f(T, MC, \text{etc.})$$

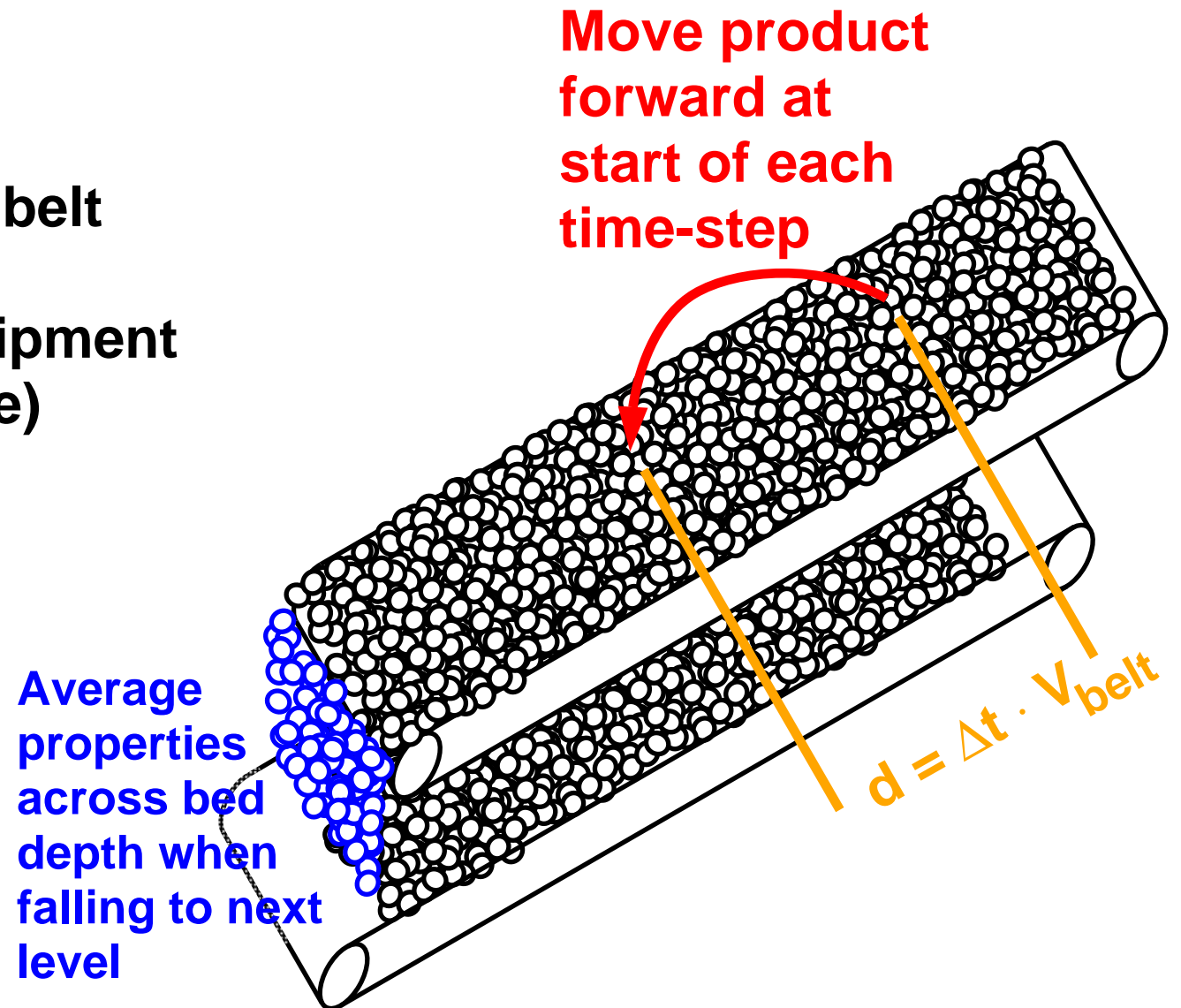
BCs: convection, water activity

Fourier's Law $k = f(T, MC, \text{etc.})$

BCs: convection, radiation,
conduction

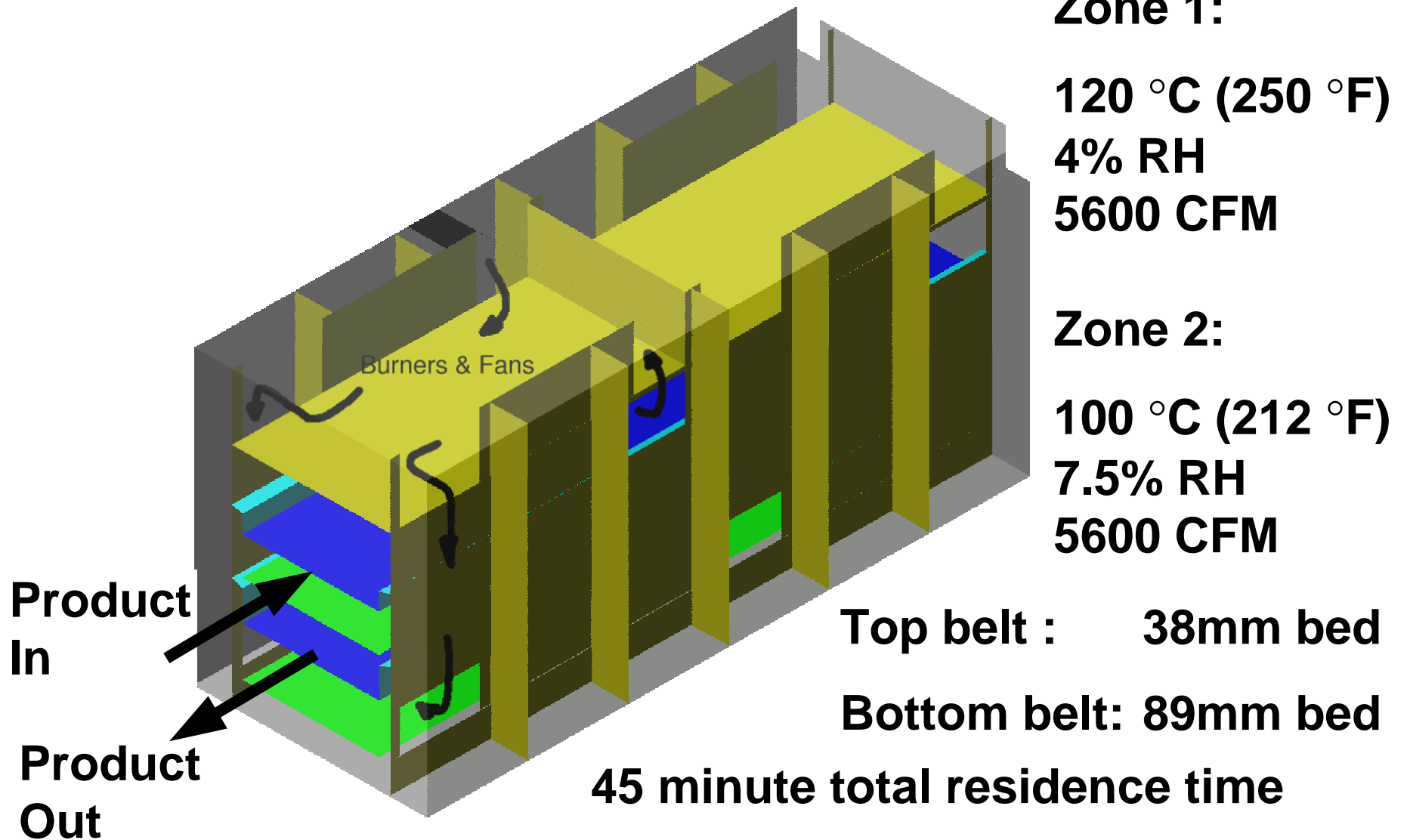
Approach - Product Movement

- Moving belt
- Drop to lower belt
- Tumbling equipment (full average)



Example Case

Two belt, two zone dryer



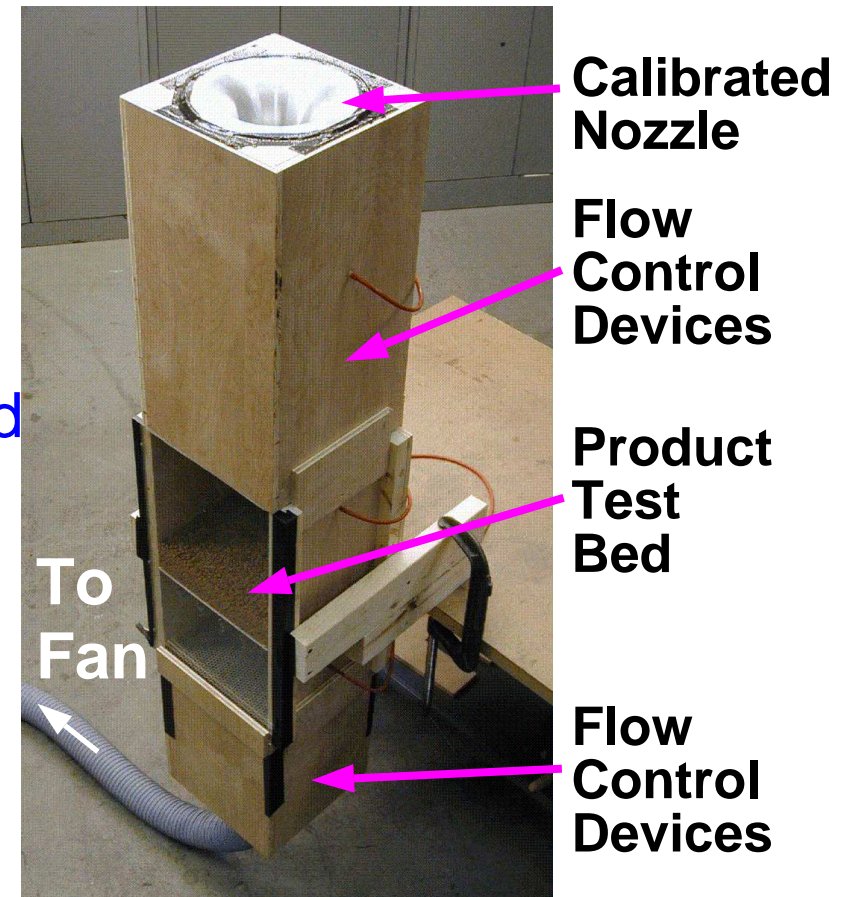
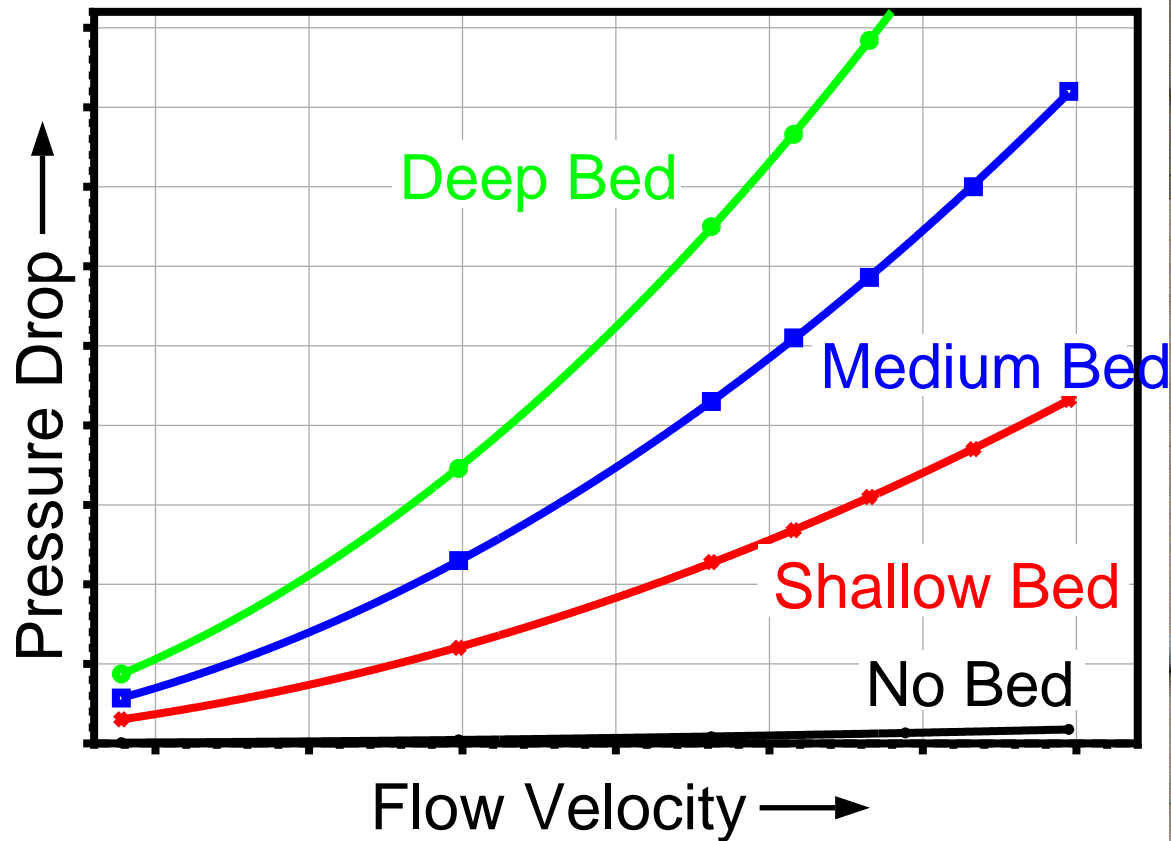
Example Case

Product details

Product flow rate:	1325 lbs/hour
Incoming temperature:	30 °C (86 °F)
Incoming moisture content:	25% (wb)
Product shape:	Spherical
Product size:	0.25" diameter
Number density:	2,728,416 pieces/m ³
Thermal conductivity:	combined solid and moisture
Liquid diffusion:	$D = D_o \cdot e^{(-K/T)}$
Water activity:	Modified Oswin's eq.

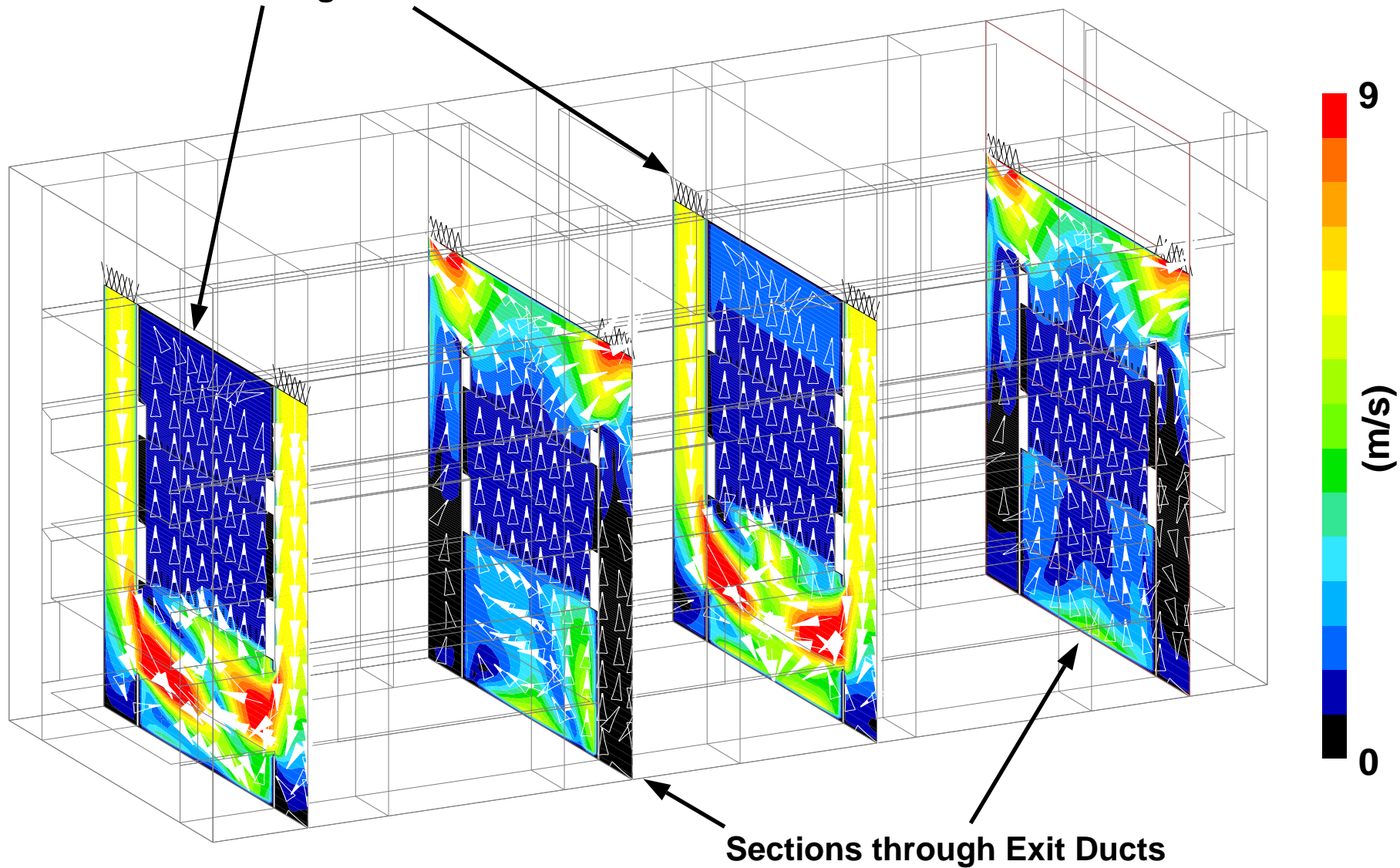
Example Case

Flow resistance of food bed

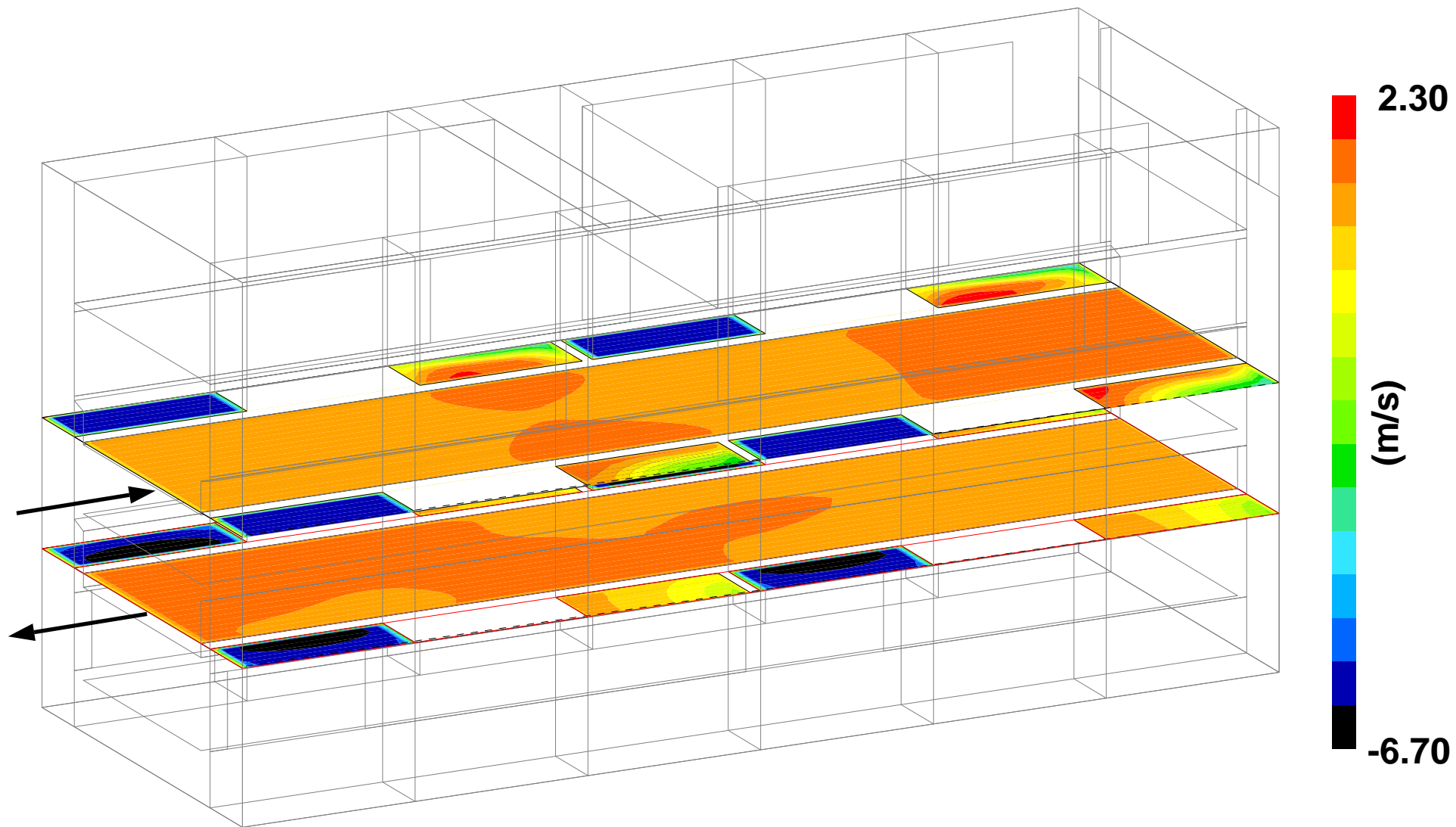


Total Velocity

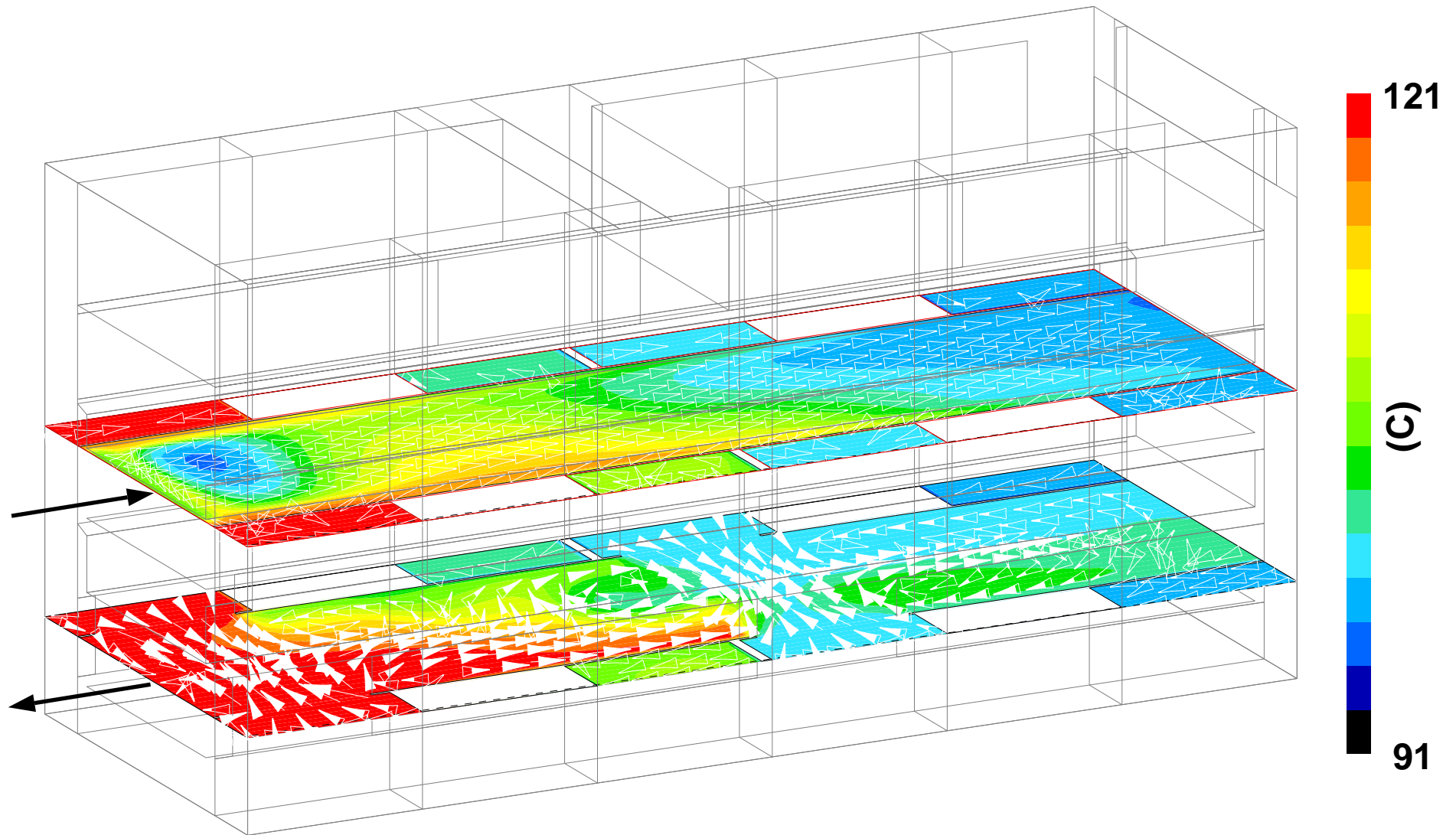
Sections through Inlet Ducts



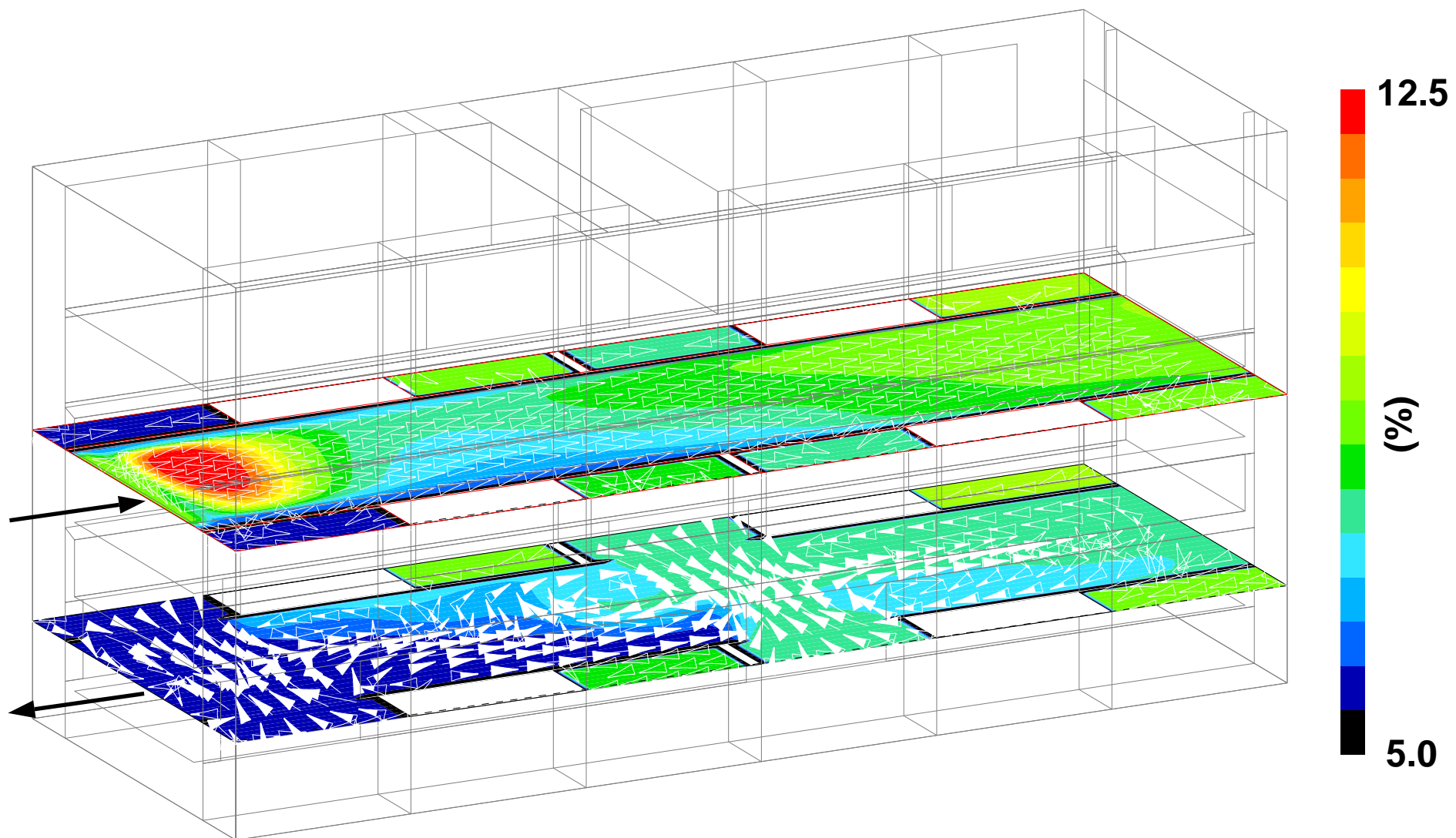
Vertical Velocity



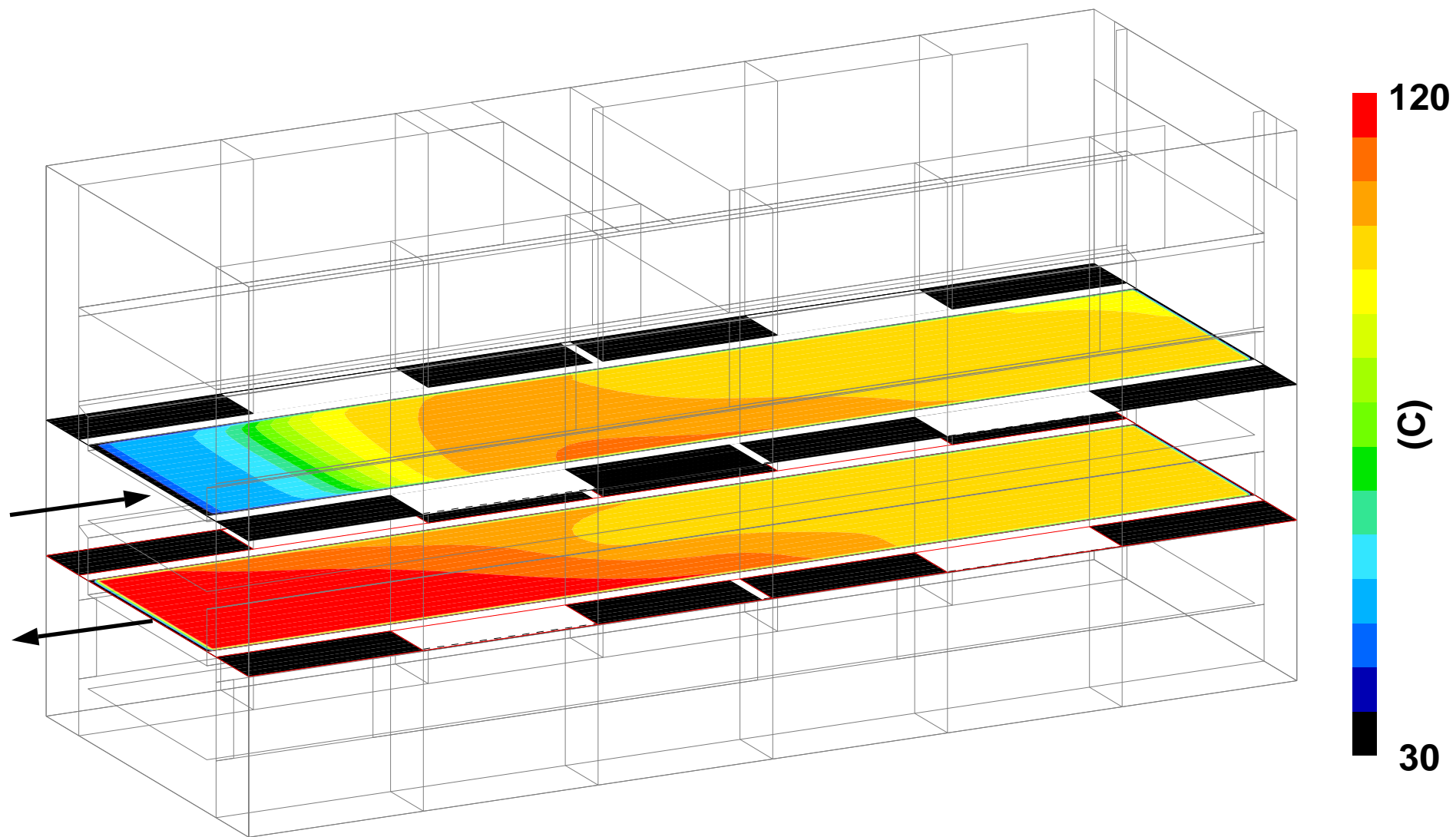
Temperature Distribution



Relative Humidity Distribution



Surface Temperature Distribution



Average Moisture Content

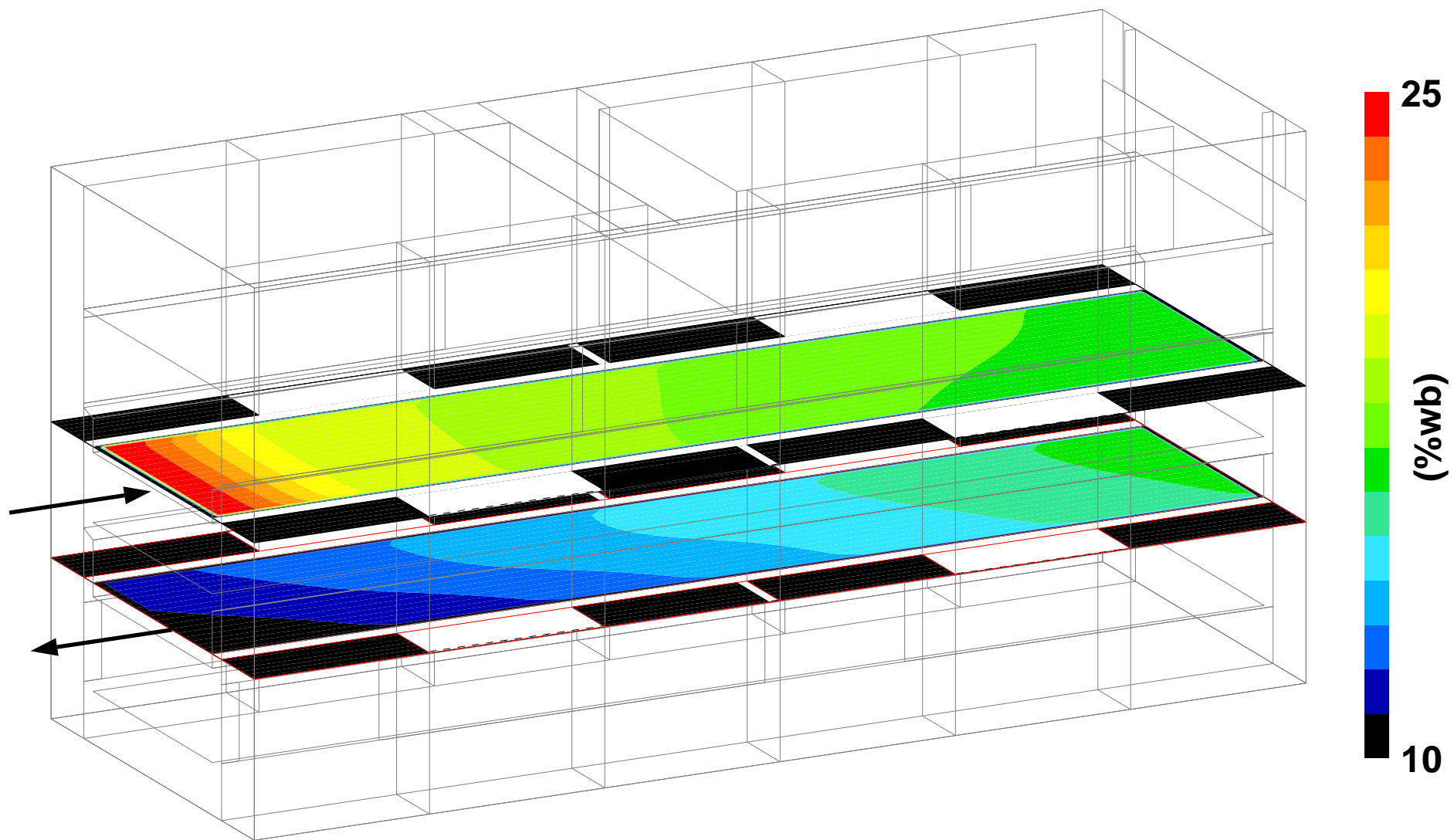
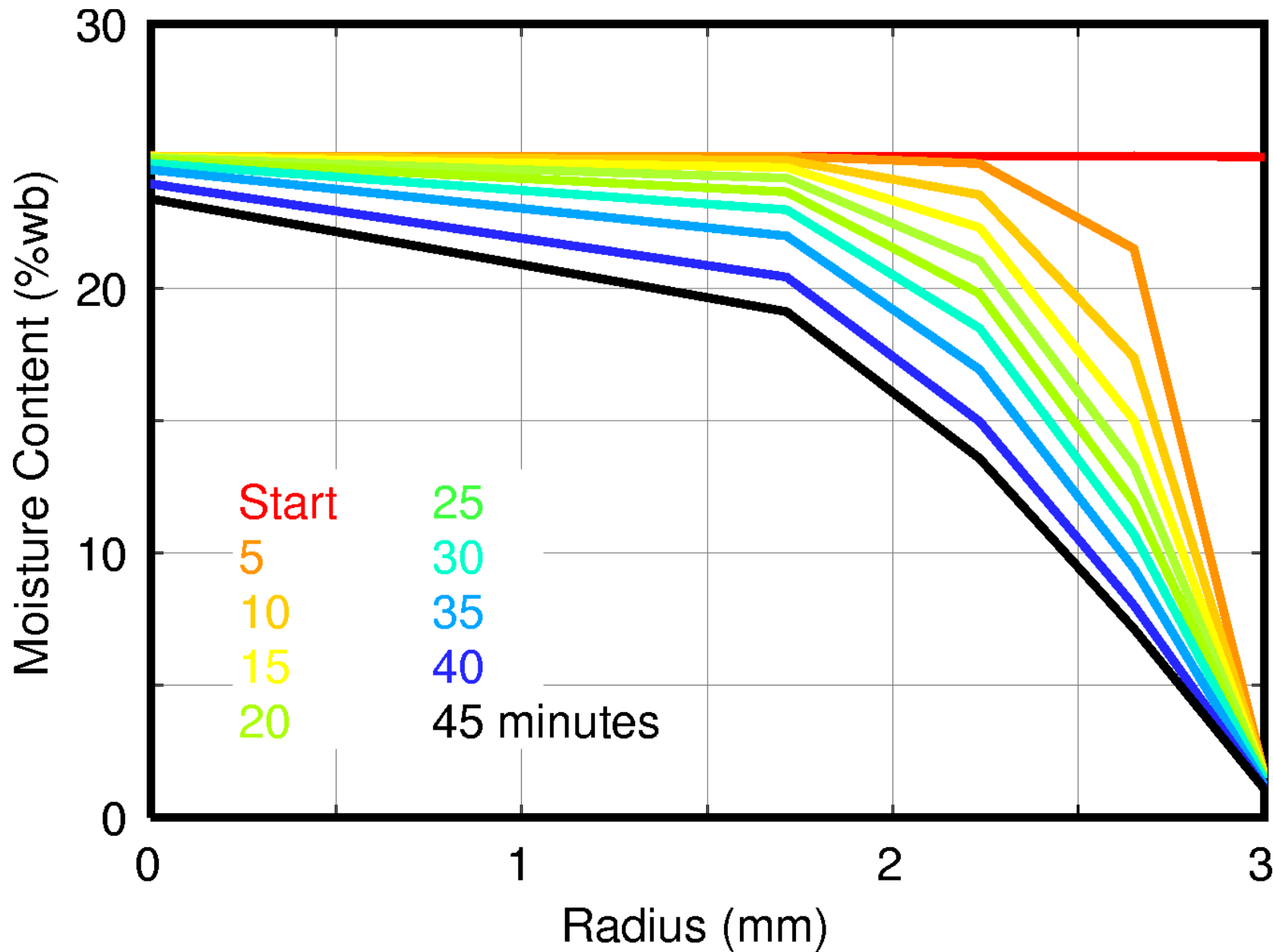
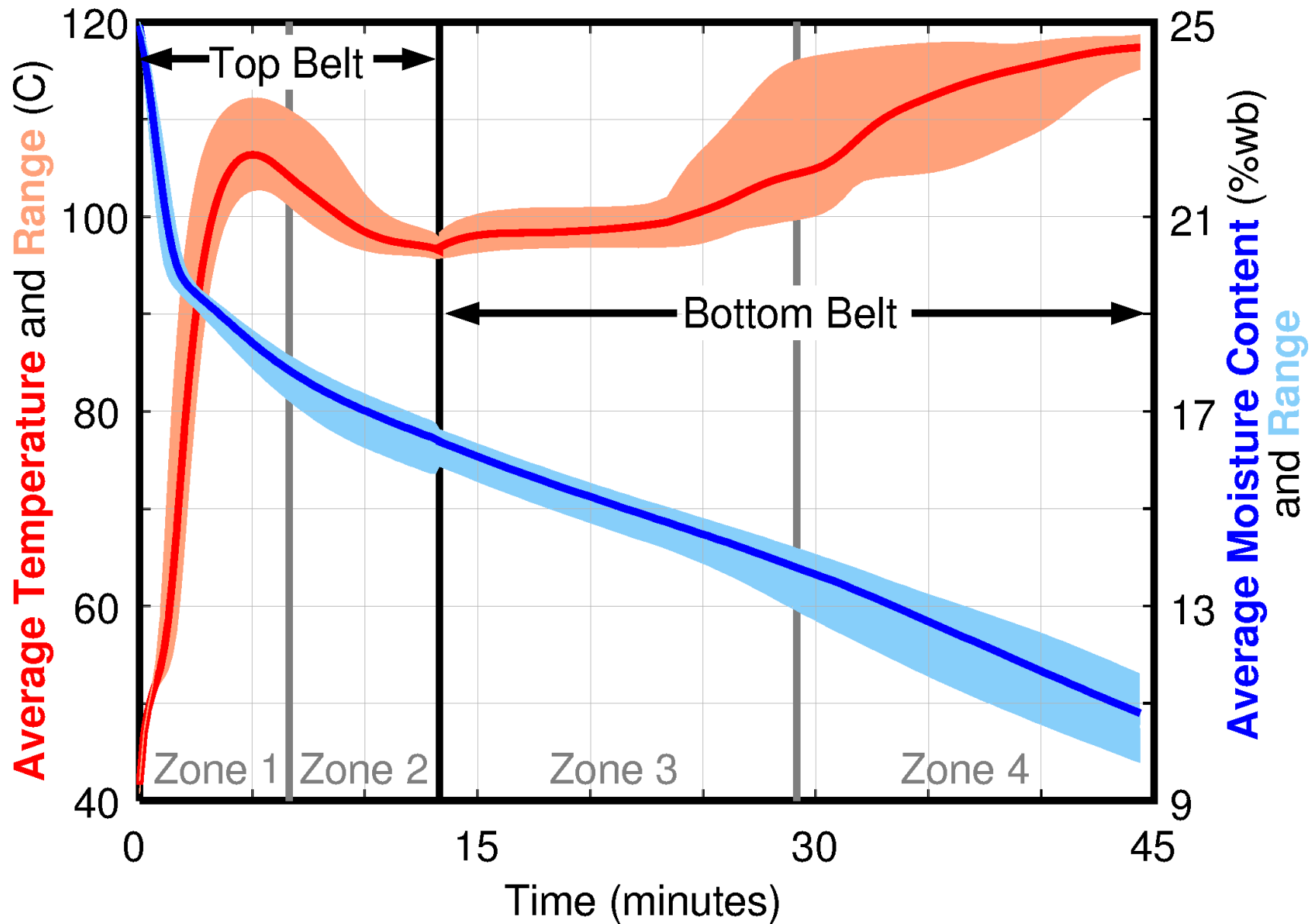


Figure 1 is a line graph showing Moisture Content (%wb) on the Y-axis (ranging from 0 to 30) versus Radius (mm) on the X-axis (ranging from 0 to 30 mm). The graph displays moisture profiles at various times: Start (red), 5 (orange), 10 (yellow), 15 (light green), 20 (green), 25 (light blue), 30 (cyan), 35 (blue), 40 (dark blue), and 45 minutes (black). The profiles show that moisture content decreases over time, with the 45-minute profile being the lowest.



Simulated Drying Curves



Validation

The coupled model approach has been validated against

- Research scale equipment**
- Production scale equipment**

Good correlation has been found

Most model adjustments were related to representation of food properties

Applications

The combined simulation approach can be applied to:

- Dryers (including coating dryers)**
- Toasting ovens**
- Roasters**
- Pasteurizers**
- Coolers**
- Non-food related processes**

Summary

- **A simulation method has been developed to analyze and improve food processing operations**
- **The approach includes most of the actual phenomena that affect the food**
- **The simulation results have been found to provide accurate results**
- **The simulation results can provide valuable insight into process operation**