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2013 NO_x-Combustion Round Table & Expo Presentations

February 18 & 19, 2013, in Salt Lake City, UT / Hosted by PacifiCorp

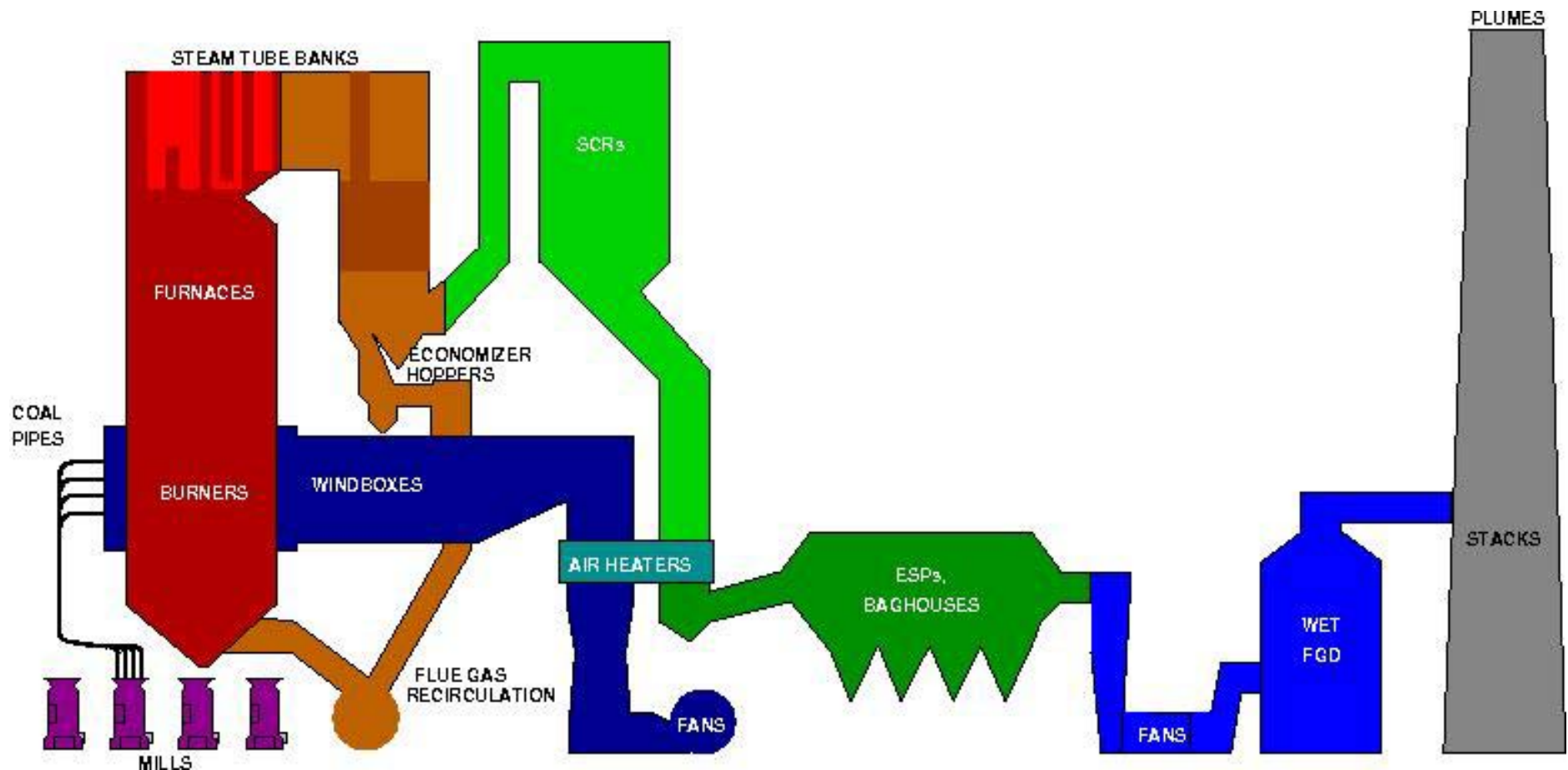
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Flow Modeling and Ash Deposition

NO_x-Combustion Round Table
February 19, 2013

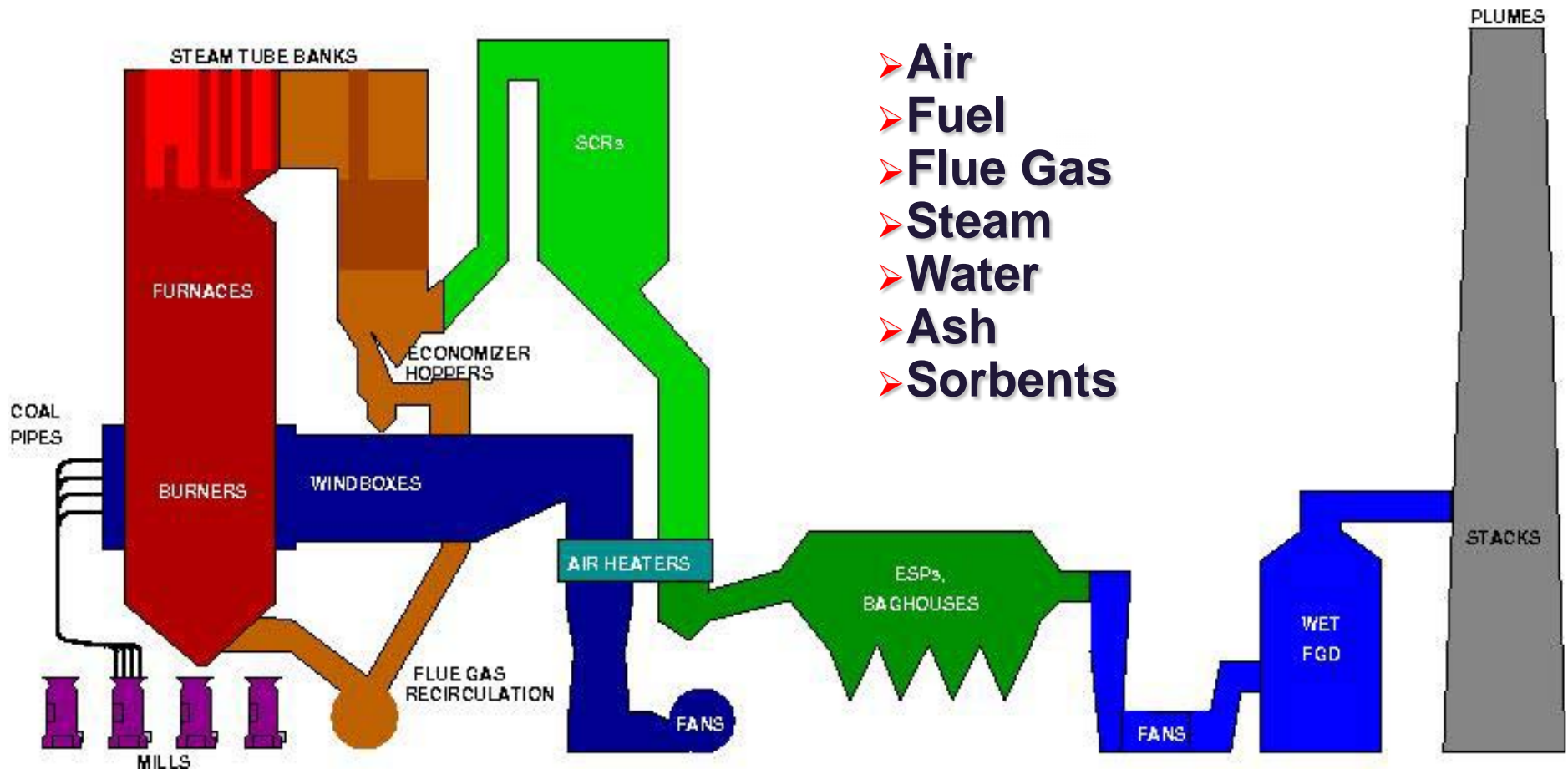
Robert Mudry, P.E.
Airflow Sciences Corporation
www.airflowsciences.com

Why Do You Care About Flow?

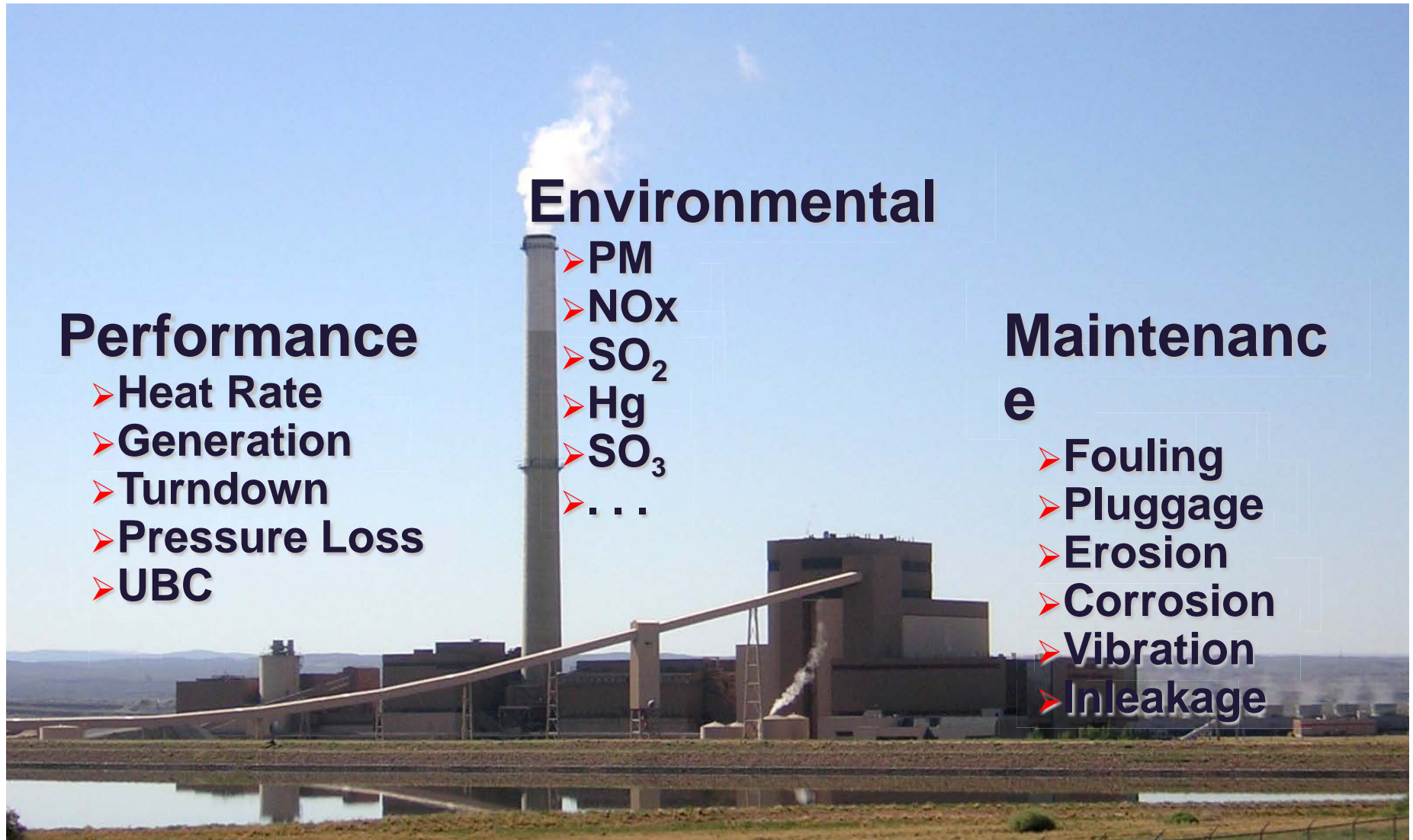


Why Do You Care About Flow?

❖ Flow is Everywhere



The Focus of Flow Optimization



Flow Analysis and Optimization Tools

❖ Field Testing

❖ Flow Modeling

- Computational Fluid Dynamics (CFD)
- Physical Flow Modeling

Field Testing

- ❖ Often used to support flow modeling efforts
 - Provide model boundary conditions
 - Collect correlation data



Field Testing

- ❖ Velocity
- ❖ Temperature
- ❖ Pressure
- ❖ Particulate
- ❖ Chemical species
- ❖ Video inspection

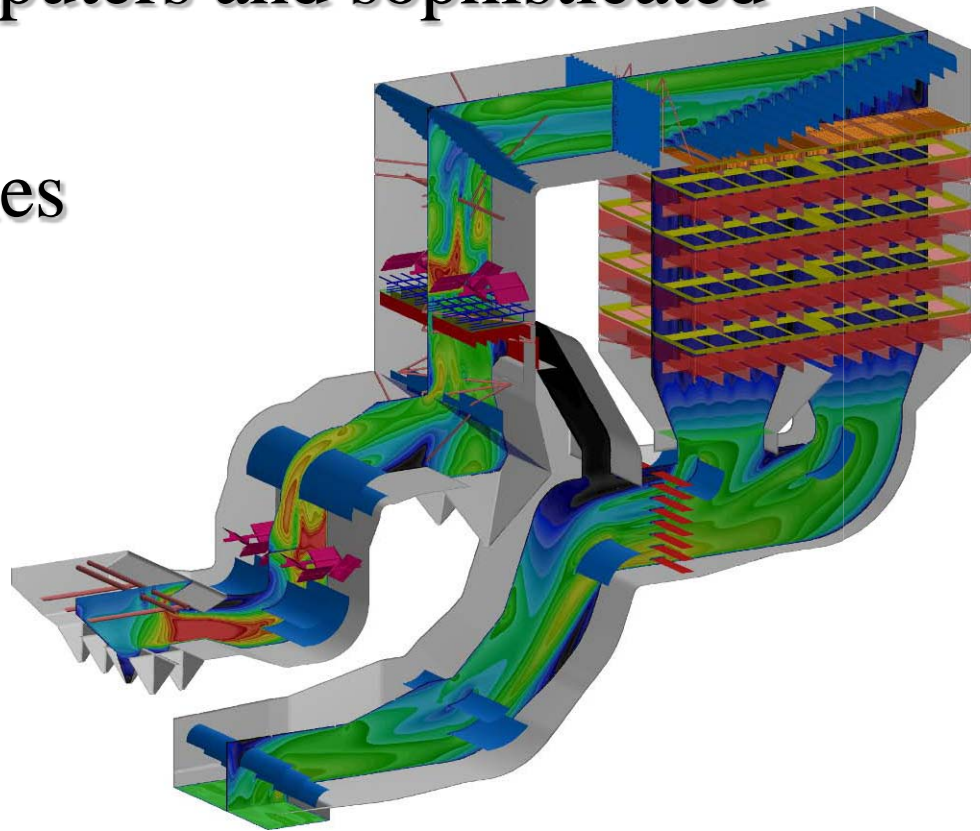


Flow Modeling

- ❖ Why perform flow modeling?
- ❖ Trial and error design optimization without modeling can work but...
 - Fixes can be costly
 - Results not as expected
 - New problems could develop
 - Modeling can save time and \$\$ in the long run
- ❖ Modeling is required for initial design of most new APC equipment
- ❖ Useful for troubleshooting / optimization of existing equipment

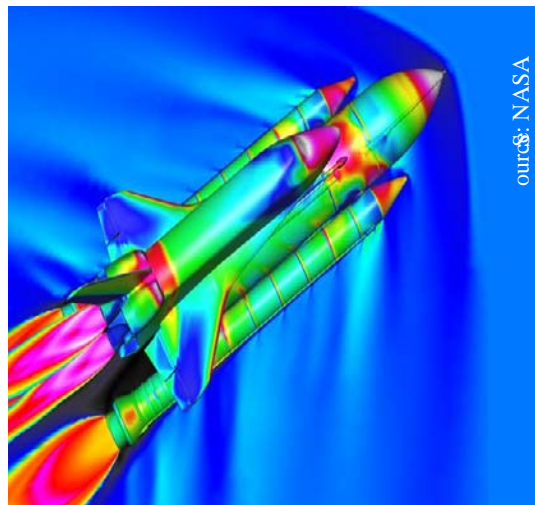
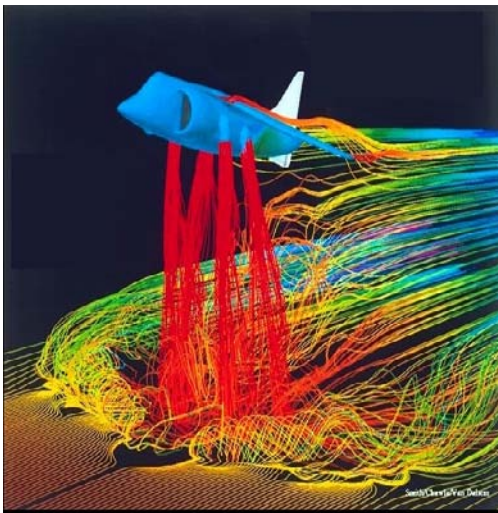
Computational Fluid Dynamics (CFD)

- ❖ Numerical simulation of flow
- ❖ Utilize high speed computers and sophisticated software
- ❖ Calculate flow properties
 - Velocity
 - Pressure
 - Temperature
 - Chemical species
 - Particle streamlines

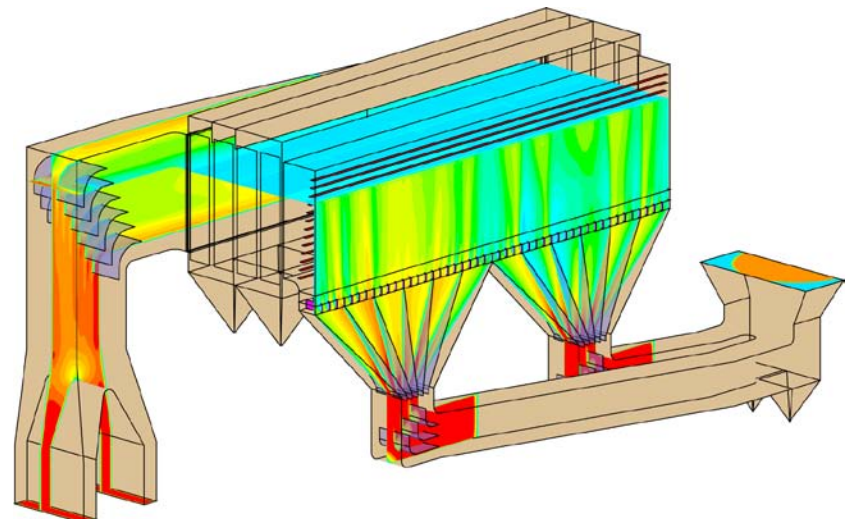


CFD History

- ❖ Developed in the aerospace industry c.1970 (with the advent of “high speed” computers)
- ❖ Applied to power plant equipment for 25+ years
- ❖ Underlying principle is to solve the first-principles equations governing fluid flow behavior



courtesy: NASA



CFD Methodology

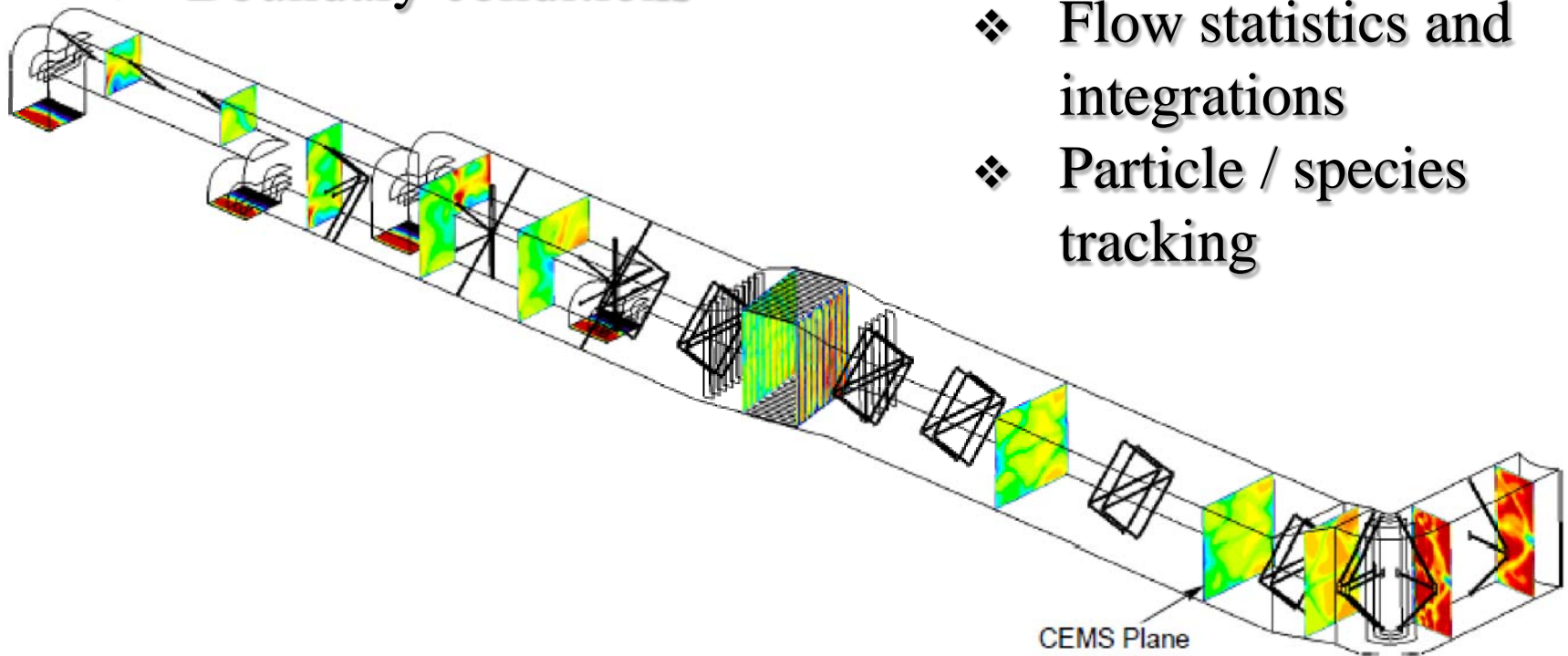
1. Set up

- ❖ Geometry (3D CAD)
- ❖ Computational mesh
- ❖ Boundary conditions

2. Solve

3. Analyze

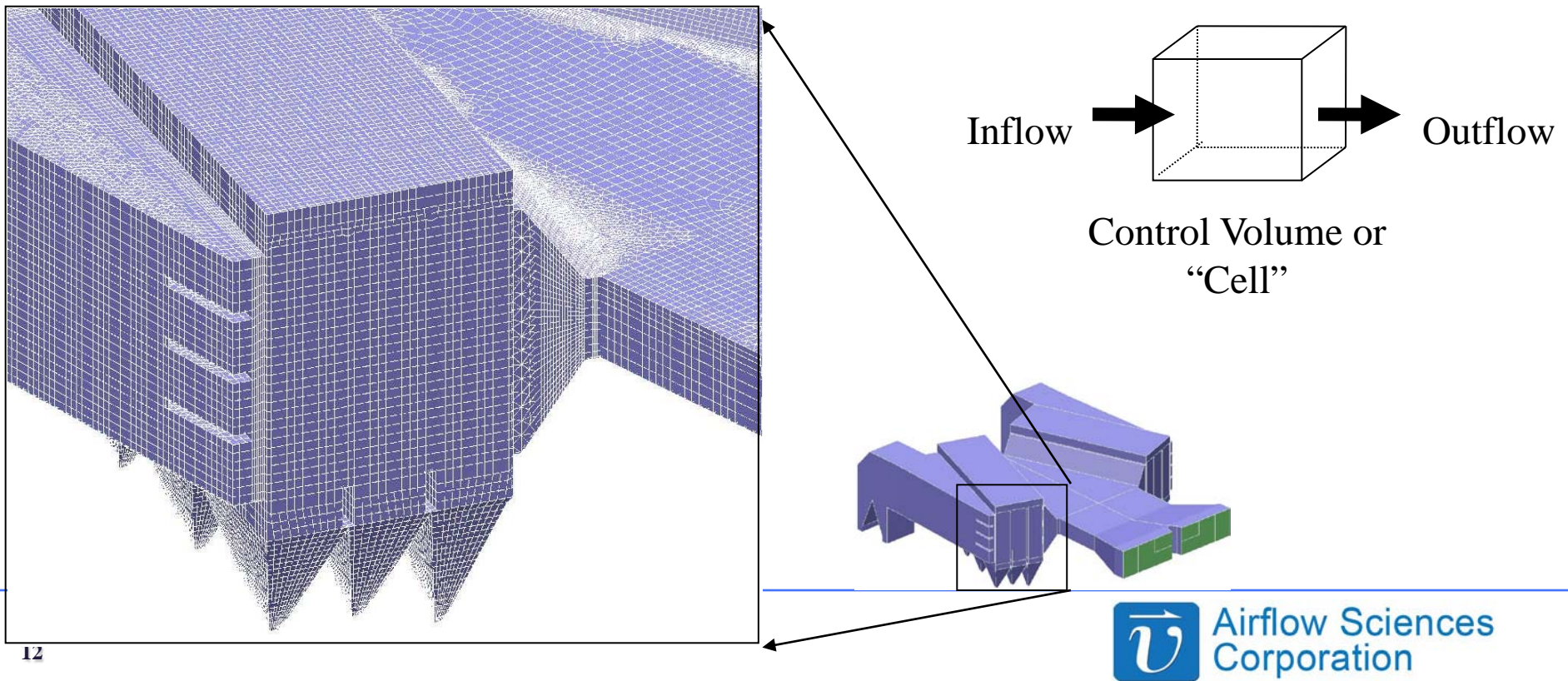
- ❖ Contour Plots
- ❖ Flow statistics and integrations
- ❖ Particle / species tracking



CFD Mesh

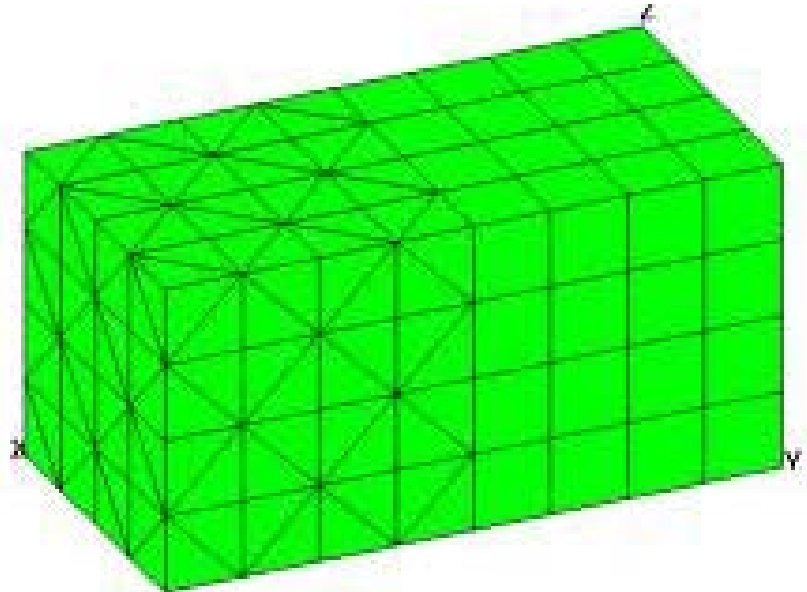
❖ Control Volume Approach

- Divide the flow domain into distinct control volumes
- Solve the Navier-Stokes equations (Conservation of Mass, Momentum, Energy) in each control volume



CFD Mesh Quality – It is Important!

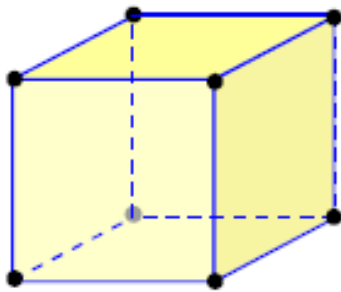
- ❖ Important mesh properties
 - ❖ Number of cells
 - ❖ Length scale of cells
 - ❖ Distribution of cells
 - ❖ Shape / topology of cells
 - ❖ Flow alignment
- ❖ Why?
 - ❖ Finer resolution = more accurate results
 - ❖ Numerical calculation scheme accuracy is influenced by cell arrangement



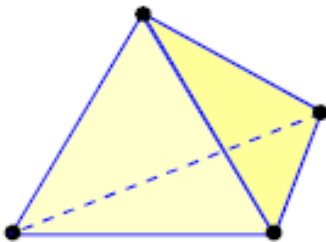
CFD Mesh Quality – Cell Topology

❖ Not all CFD cells are created equal

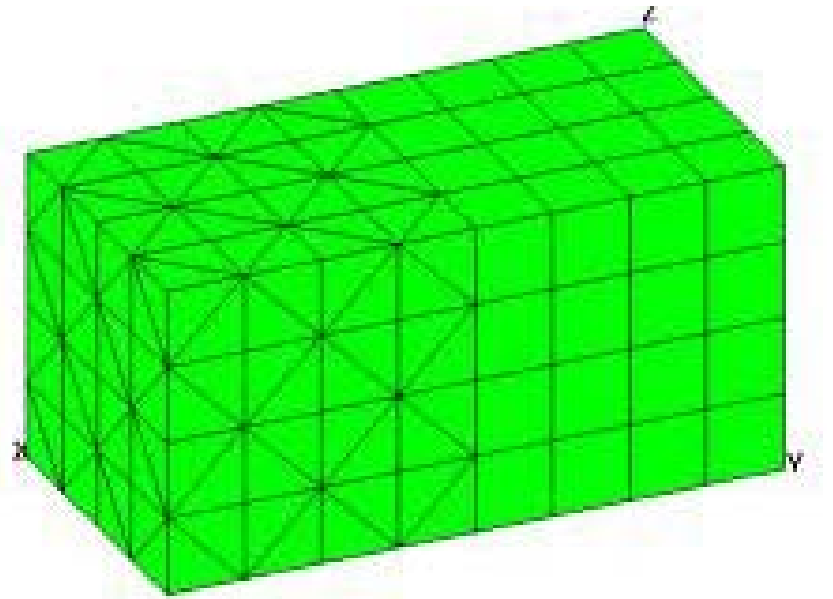
❖ 5 million Hex cells = 20 million Tet cells



Hexahedral cell
(6 faces)

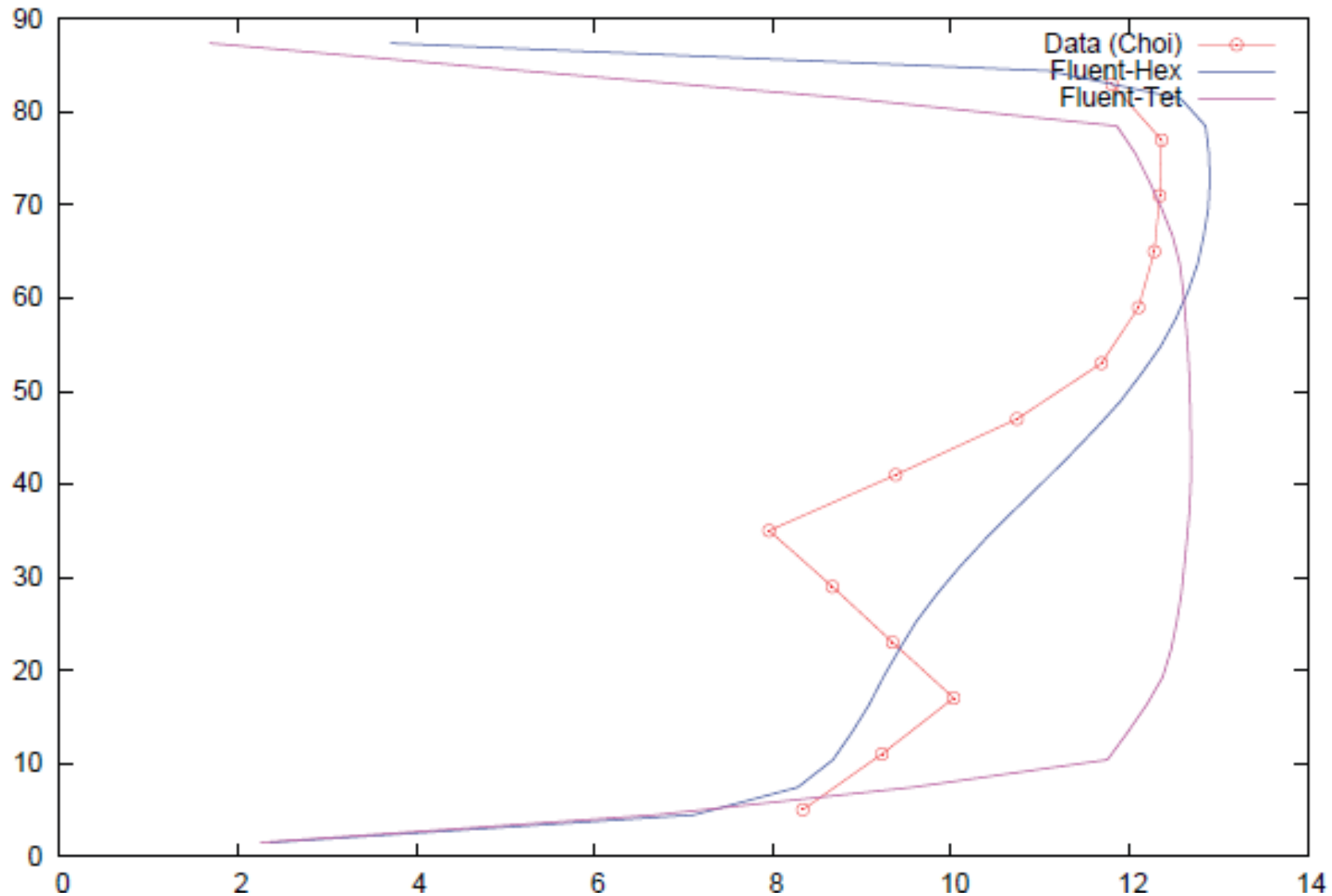


Tetrahedral cell
(4 faces)



Why? 4 Tet cells fit into 1 Hex cell of the same length scale

CFD Mesh Quality – Tet vs. Hex



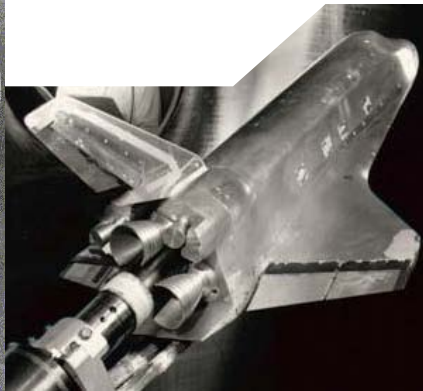
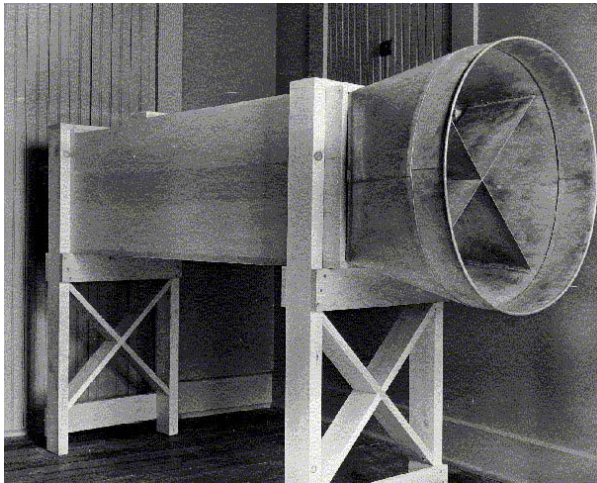
Physical Flow Modeling

- ❖ Lab representation of geometry
- ❖ Typical scale 1:8 to 1:16
- ❖ “Cold flow” modeling
- ❖ Visualize flow with smoke
- ❖ Simulate ash re-entrainment
- ❖ Measure flow properties
 - Velocity
 - Pressure
 - Tracer gas



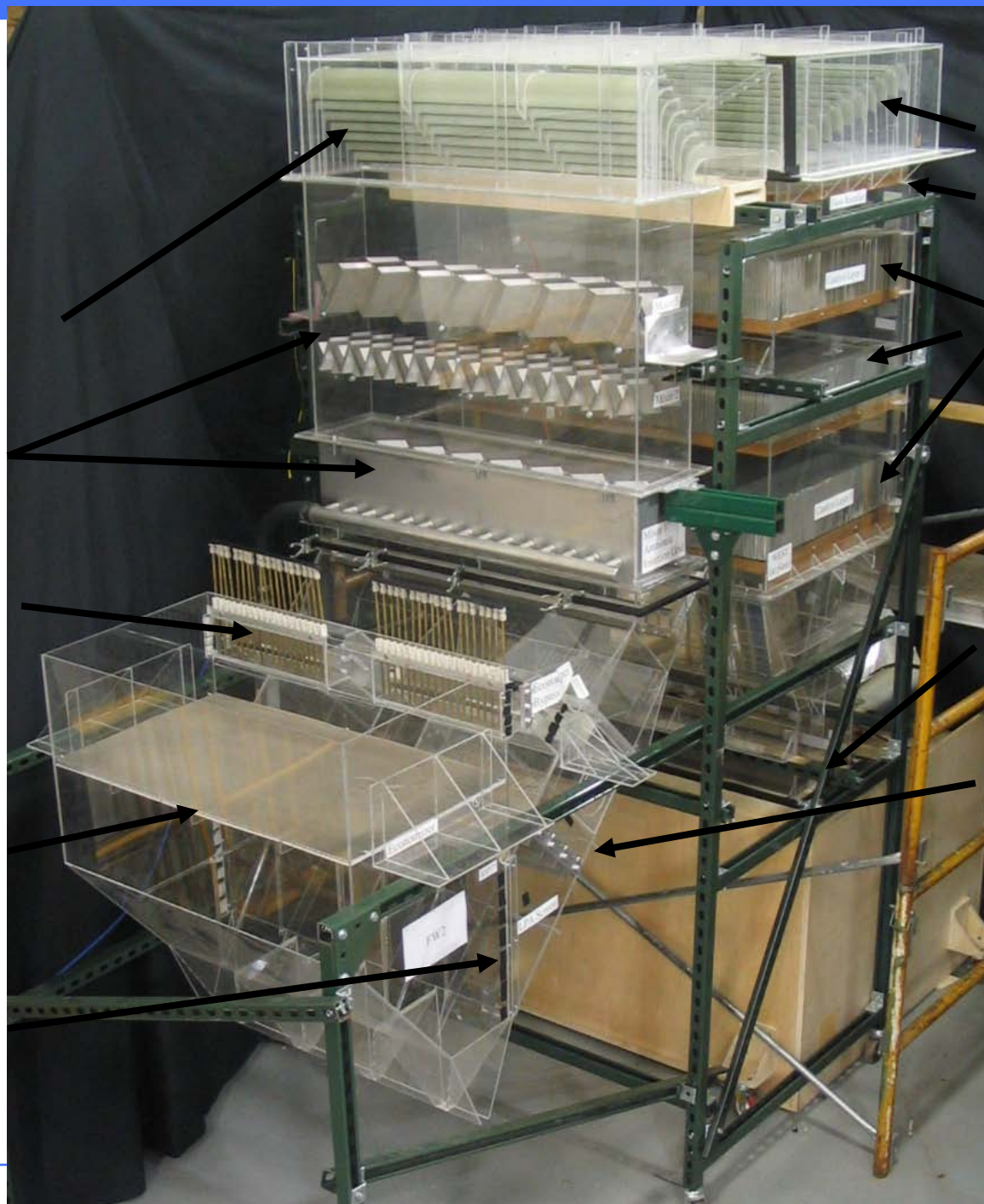
Physical Modeling History

- ❖ Utilized for fluid flow analysis for a century ... or more?
- ❖ Applied to power plant equipment for decades
- ❖ Underlying principle is to reproduce fluid flow behavior in a controlled, laboratory environment



Typical 1/12 scale physical model - SCR

- Turning vanes
- AIG w/static mixers
- Economizer bypass
- Economizer outlet
- LPA screen



- Vanes
- Rectifier
- Catalyst layers
- Air heater
- Dampers

Physical Model Methodology

❖ Key criteria is to generate “Similarity” between the scale model and the real-world object

- Geometric similarity

- Accurate scale representation of geometry
- Inclusion of all influencing geometry elements
- Selection of scale can be important

- Fluid dynamic similarity

- Precise Reynolds Number (Re) matching is not feasible
- General practice is to match full scale velocity but ensure that Re remains in the turbulent range throughout the model

$$Re = \frac{\rho v D_h}{\mu}$$

Physical Model Methodology

1. Set up

- ❖ Fabricate (from CAD)
- ❖ Boundary conditions
- ❖ Similarity calculations



2. Test

3. Analyze

- ❖ Contour plots
- ❖ Flow statistics and integrations
- ❖ Flow visualization

Flow Modeling Pros and Cons

❖ Physical Modeling - Pros

- Proven technique
- Can “touch and feel”
- Complex flow simulations and solutions
- NH_3 distribution modeling
- Ash dropout / re-entrainment
- Flow visualization

❖ Physical Modeling - Cons

- Iterations can be time consuming (no parallelization)
- Thermal mixing difficult
- Measurement points limited
- Cannot simulate complex physics (reactions, density variation)
- Model storage can take up significant space

Flow Modeling Pros and Cons

❖ CFD Modeling - Pros

- Iterations can be done in parallel
- Detailed representation of flow and mixing patterns
- Data available at millions of traverse points
- Output can be customized to maximize information
- Can track particulate in flight
- Model storage is simple

❖ CFD Modeling - Cons

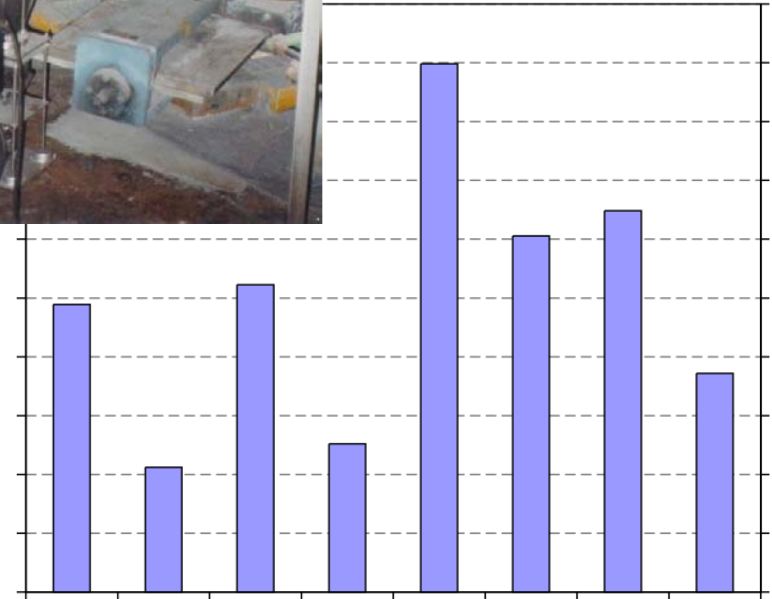
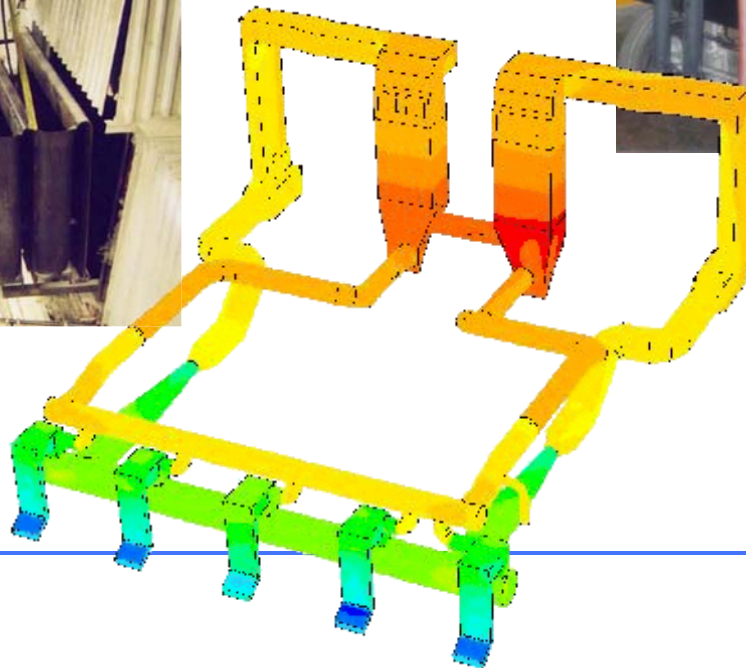
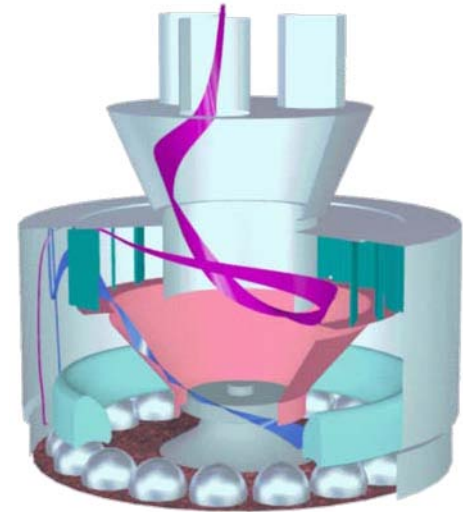
- Model is virtual, no “touch and feel” comfort
- Accuracy of results relies on mesh quality and size
- Particulate dropout/re-entrainment modeling is limited
- NH_3 distribution modeling requires detailed mesh
- Some physics and geometries are difficult to resolve in mesh

Flow Model Applications

- ❖ Primary Air / Coal Flow
- ❖ Windboxes / Secondary Air
- ❖ Furnaces
- ❖ ESPs
- ❖ Fabric Filters
- ❖ FGD
- ❖ Sorbent Injection
- ❖ SCR_s

Primary Air / Coal Flow Balancing

- ❖ Optimize combustion
 - Balance PA flows
 - Equal coal flow per burner
 - Adequate fineness
- ❖ Modeling and testing

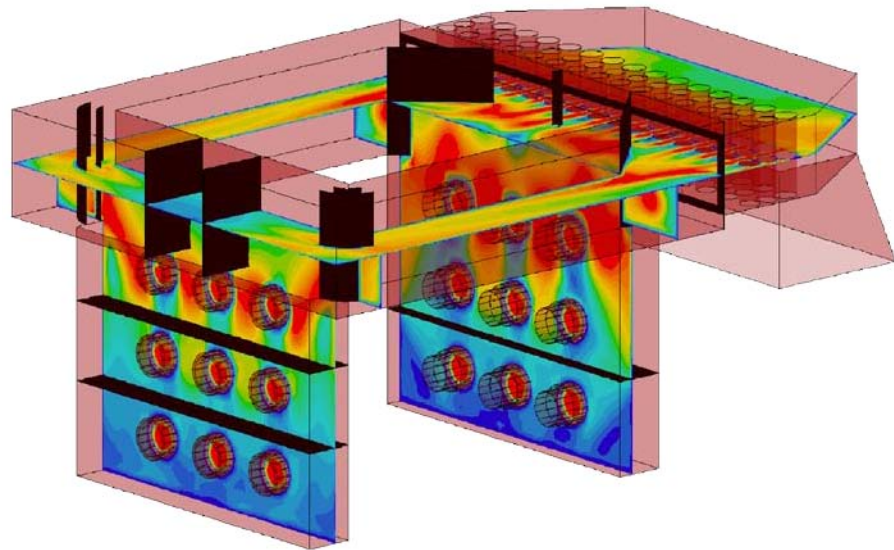
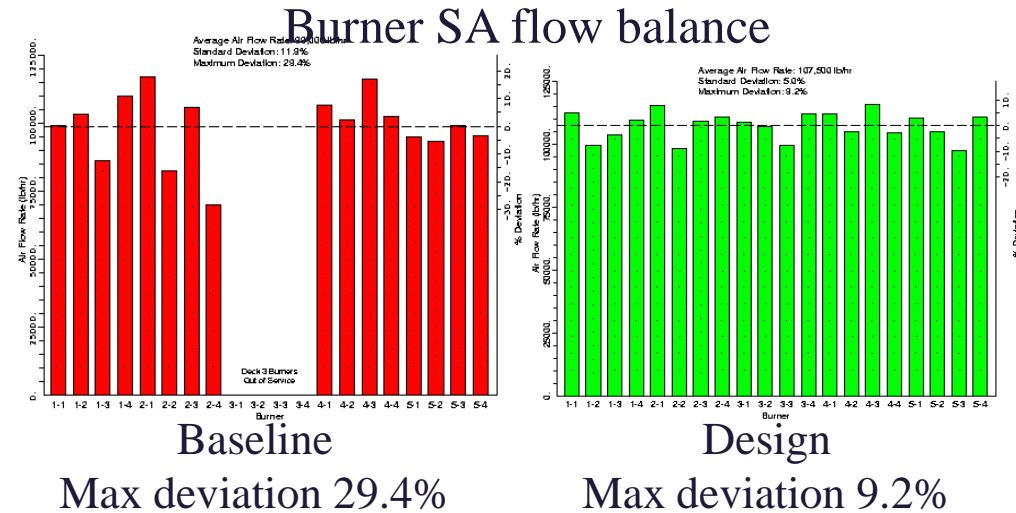


Windbox Flow Balancing

❖ Optimize combustion

- Balance secondary air
- Control flow entering burner (ram air effect)

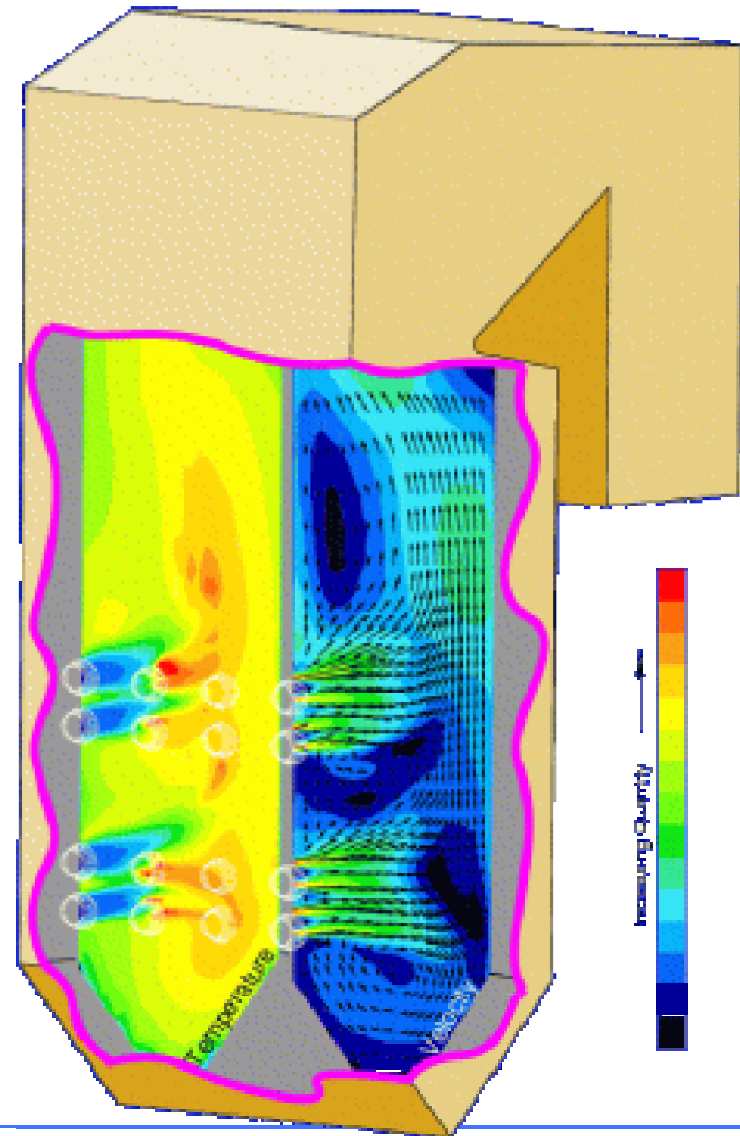
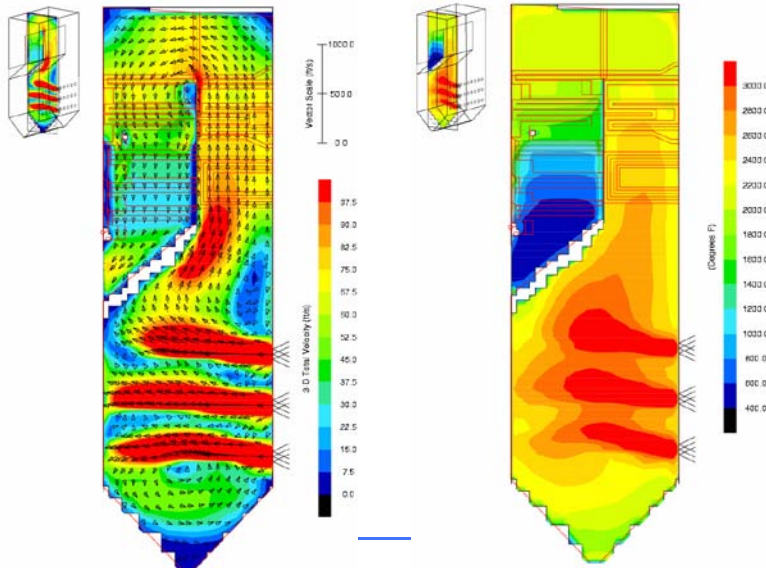
❖ Modeling and testing



Furnace Combustion Optimization

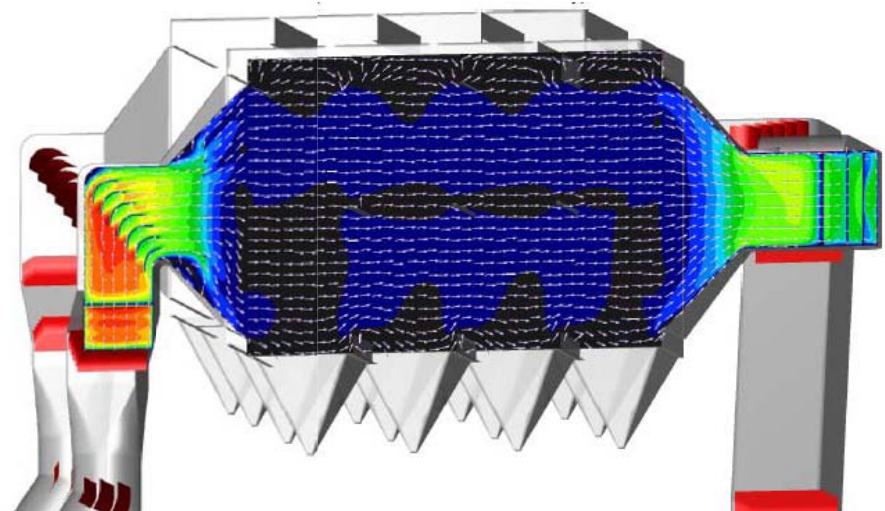
❖ Typical goals

- Reduce NOx
- Minimize UBC
- Improve heat transfer
- Avoid corrosion
- Decrease slagging



ESP Flow Optimization

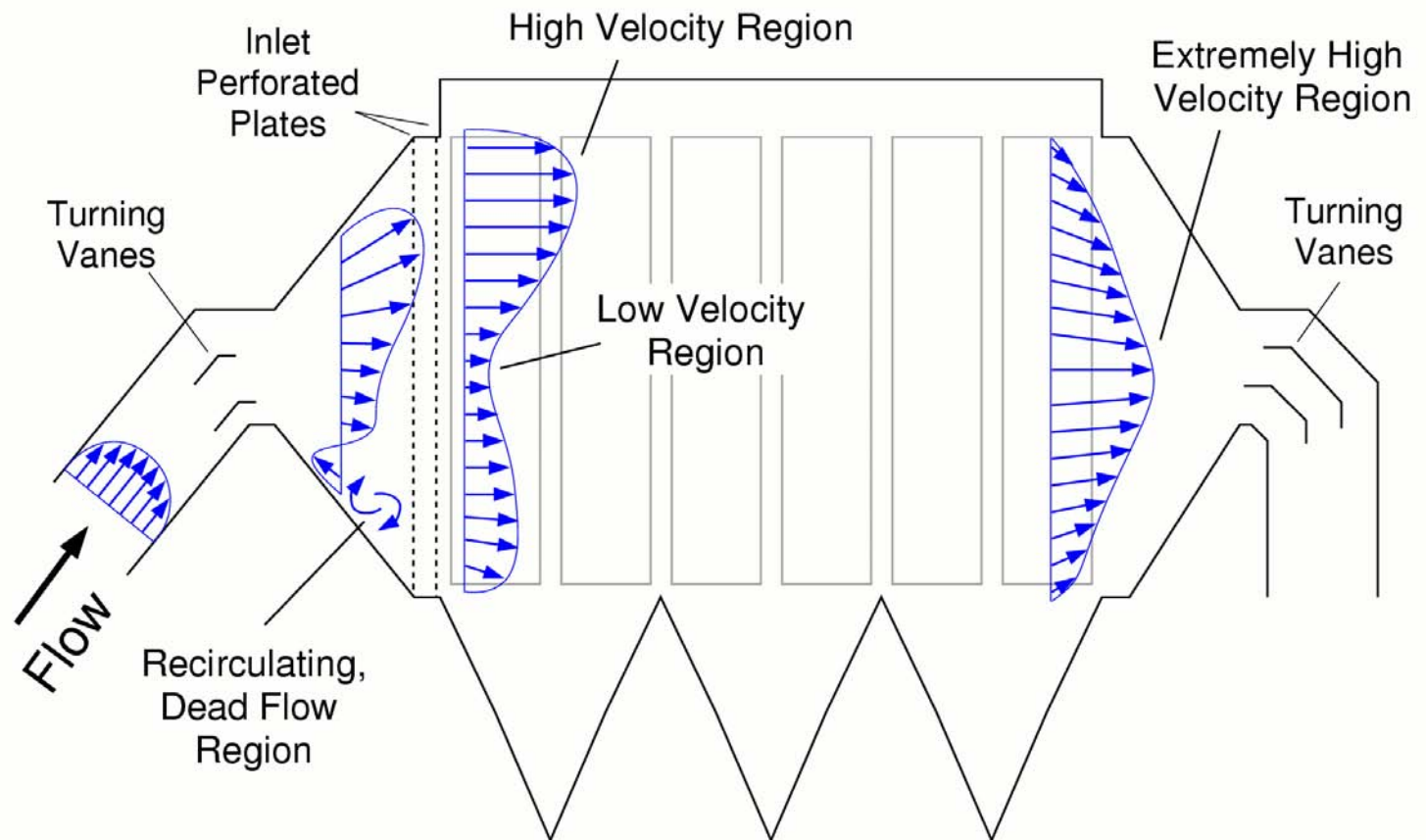
- ❖ Flow distribution
- ❖ Flow balance between cells
- ❖ Pressure loss
- ❖ Thermal mixing
- ❖ Gas conditioning
- ❖ Ash deposition



ESP Velocity Distribution

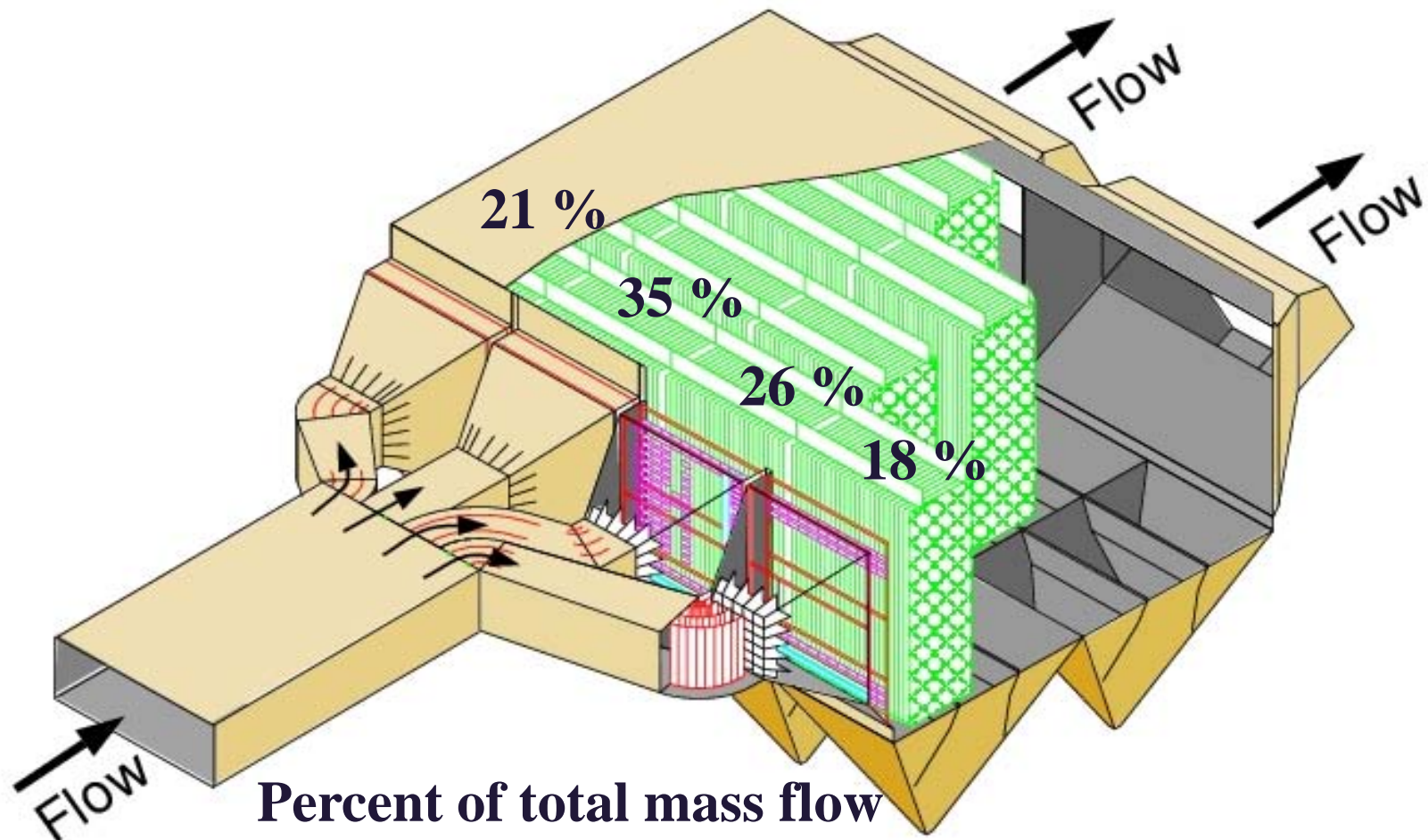
- ❖ Uniform velocity within collection region
- ❖ Industry standards

- ICAC
- % RMS deviation



Gas Flow Balance

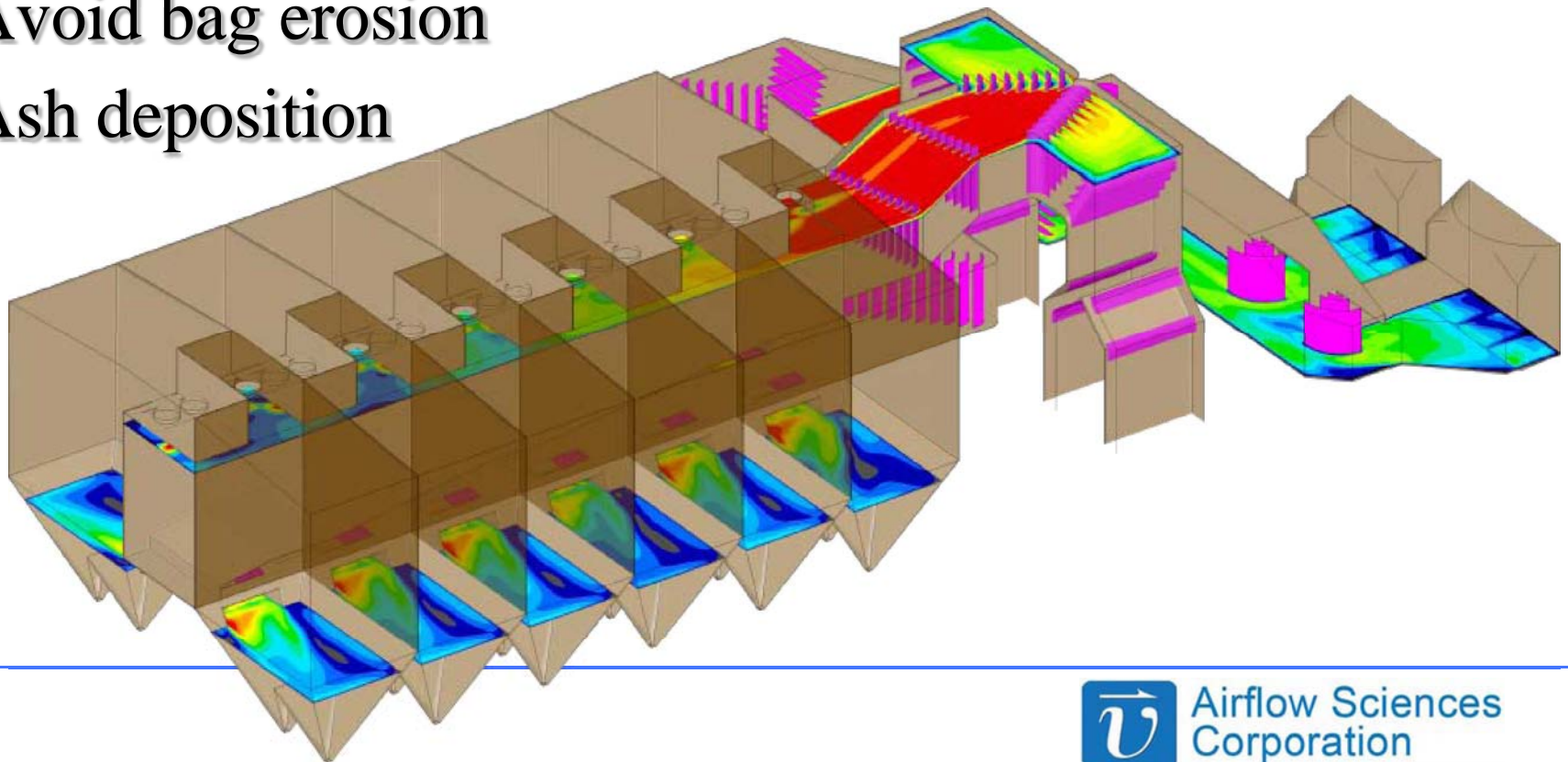
❖ Industry standard +/- 10% deviation



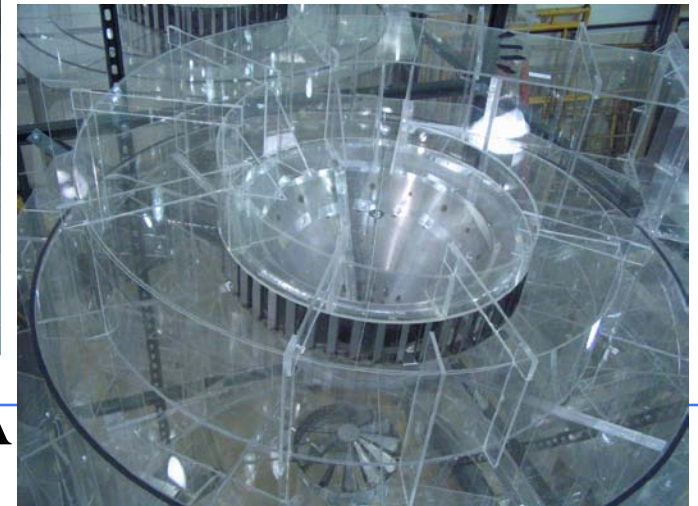
**Percent of total mass flow
through each chamber**

Fabric Filter Flow Modeling

- ❖ Uniform velocity distribution and equal balance between compartments
- ❖ Compartments out-of-service
- ❖ Avoid bag erosion
- ❖ Ash deposition



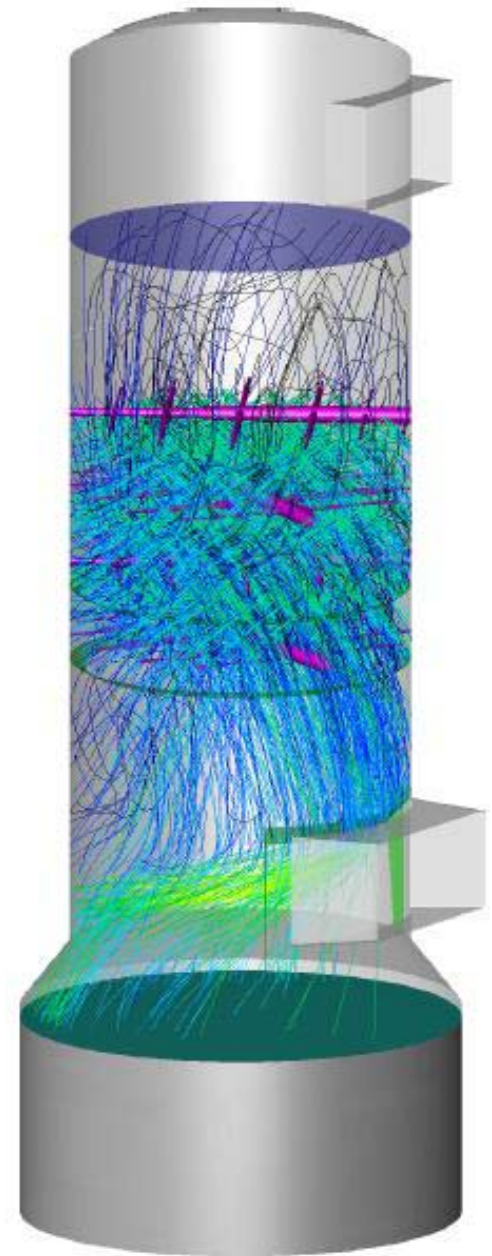
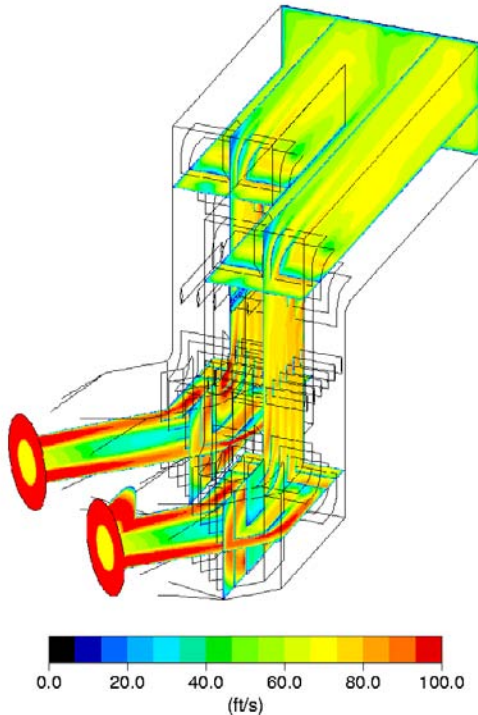
Fabric Filter Flow Modeling



FF with SDA

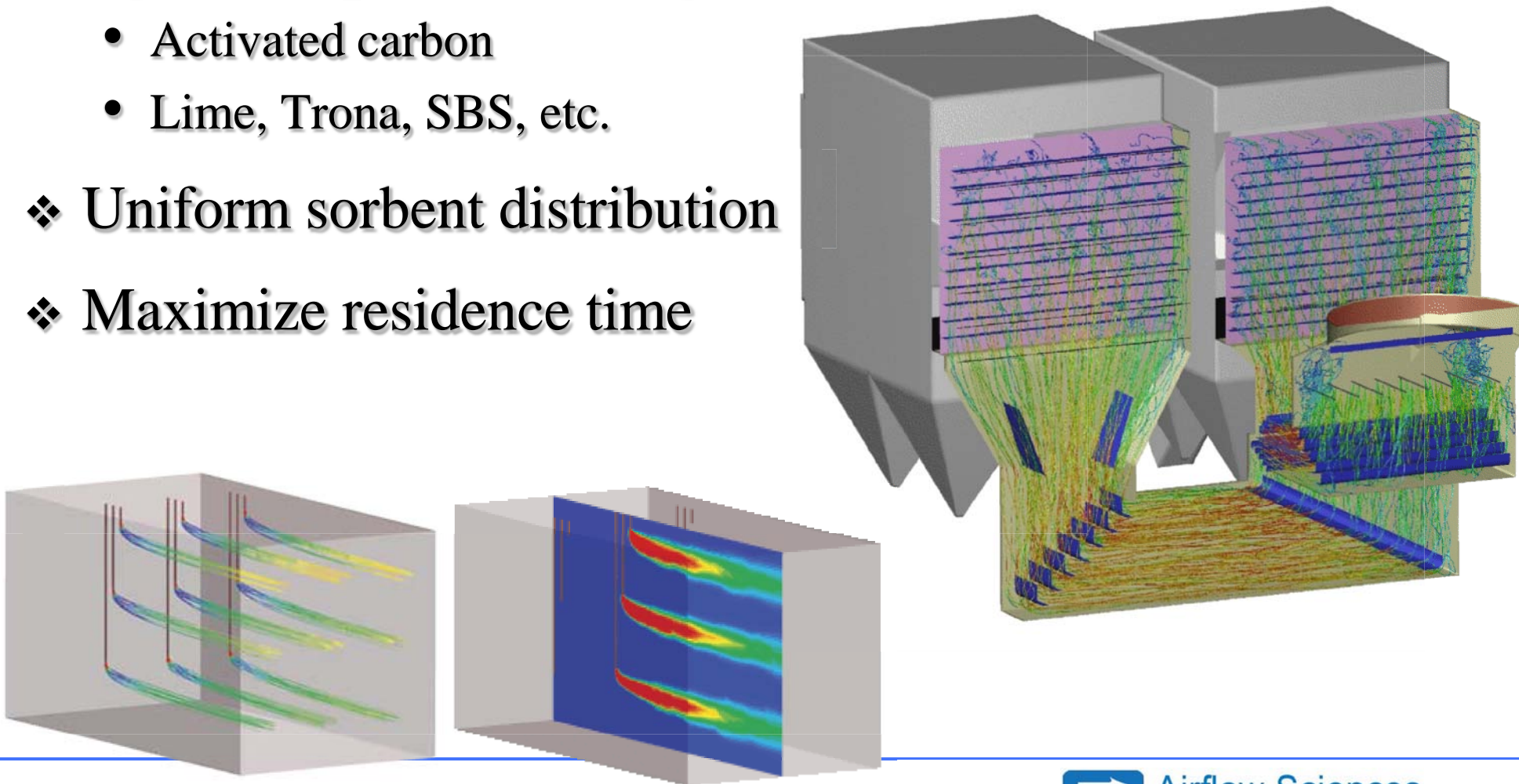
Wet FGD Flow Modeling

- ❖ Flow distribution
- ❖ Water droplet behavior
- ❖ Pressure loss
- ❖ Solids deposition



Mercury / SO₃ Reduction

- ❖ Injection upstream of baghouse or ESP
 - Activated carbon
 - Lime, Trona, SBS, etc.
- ❖ Uniform sorbent distribution
- ❖ Maximize residence time



SCR Flow Optimization

- ❖ Velocity distribution
- ❖ Thermal mixing
- ❖ NO_x profile / mixing
- ❖ Ammonia injection
- ❖ Pressure loss
- ❖ Large particle ash (LPA) capture
- ❖ Ash deposition



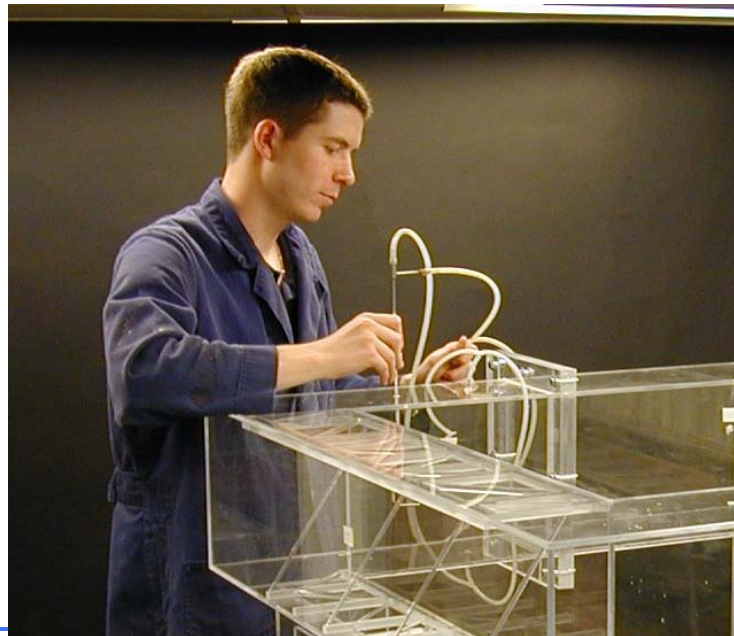
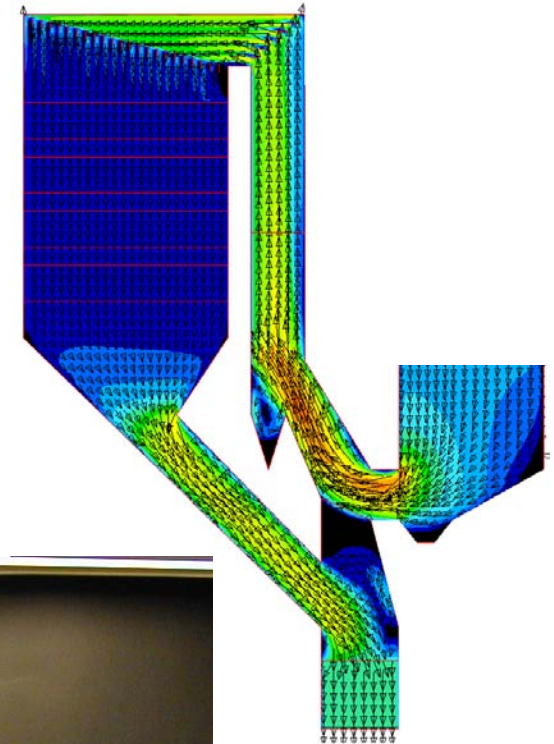
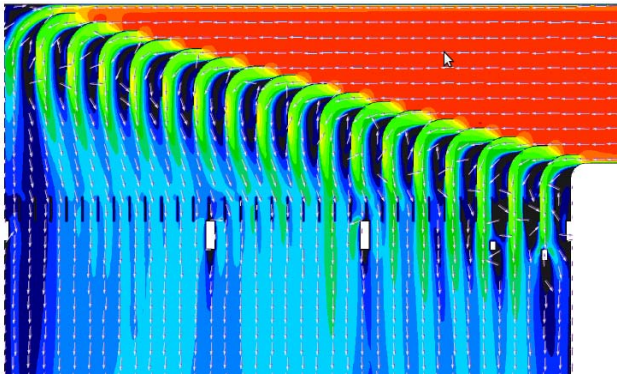
SCR Velocity Distribution

❖ Uniform velocity profile

- At ammonia injection grid
- At catalyst inlet
- At air heater inlet

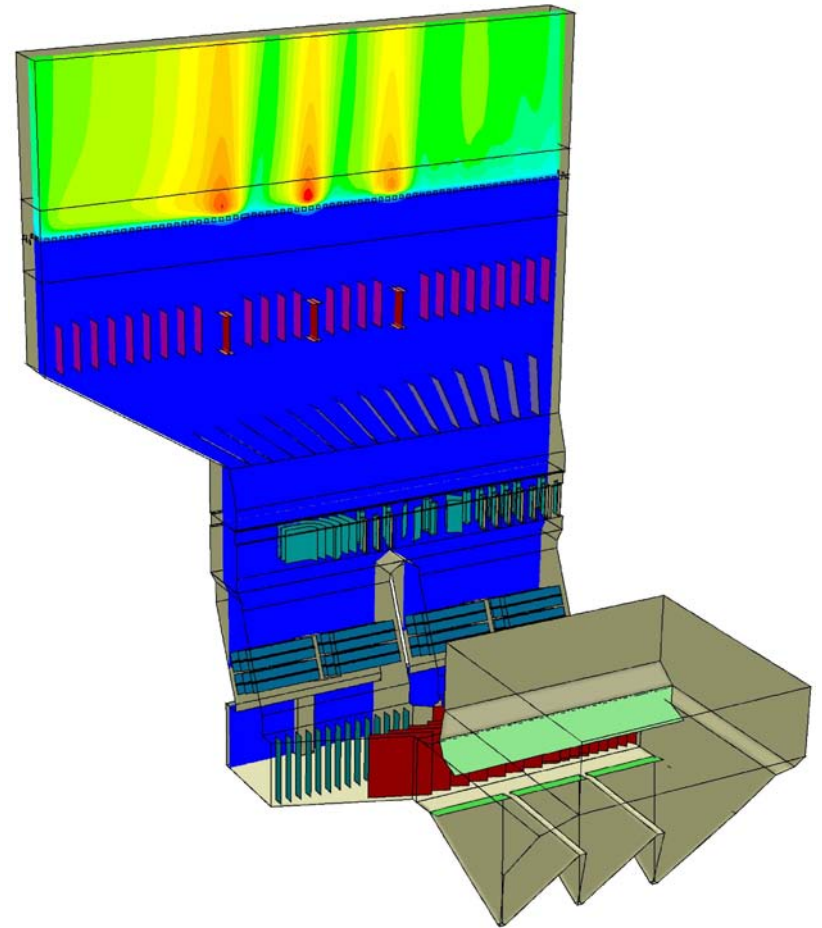
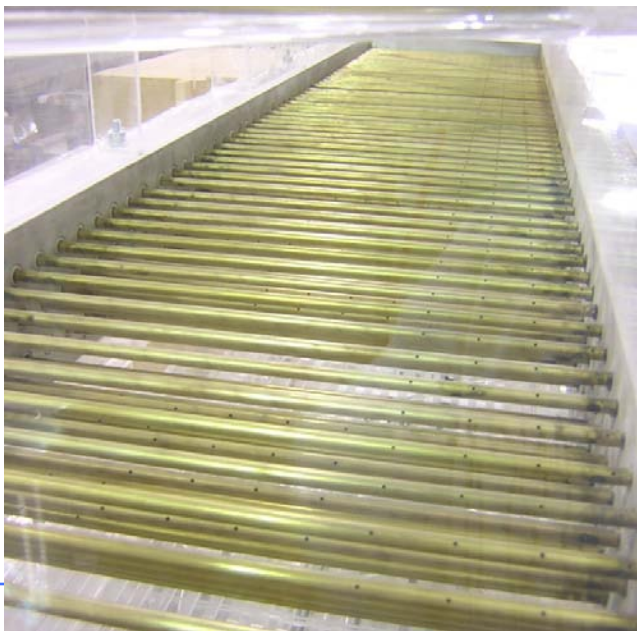
❖ Minimal angularity

- At catalyst inlet



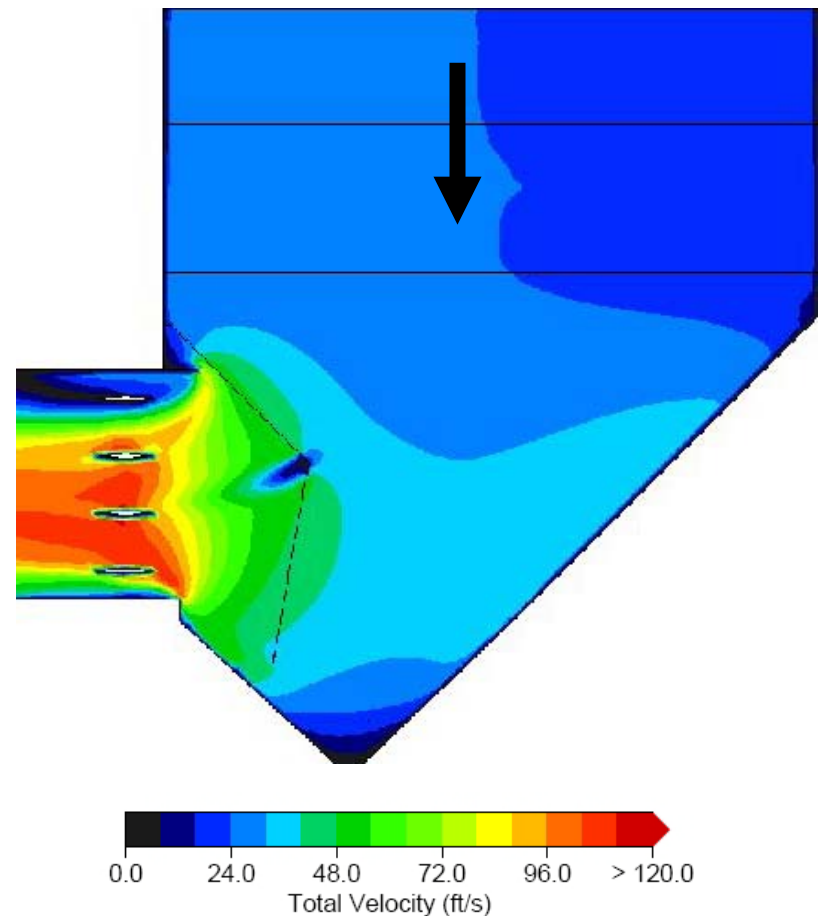
SCR Ammonia Injection

- ❖ Desire uniform NH_3 -to- NO_x ratio at catalyst
- ❖ Tracer gas used to represent flows in physical model
- ❖ Track gas species in CFD



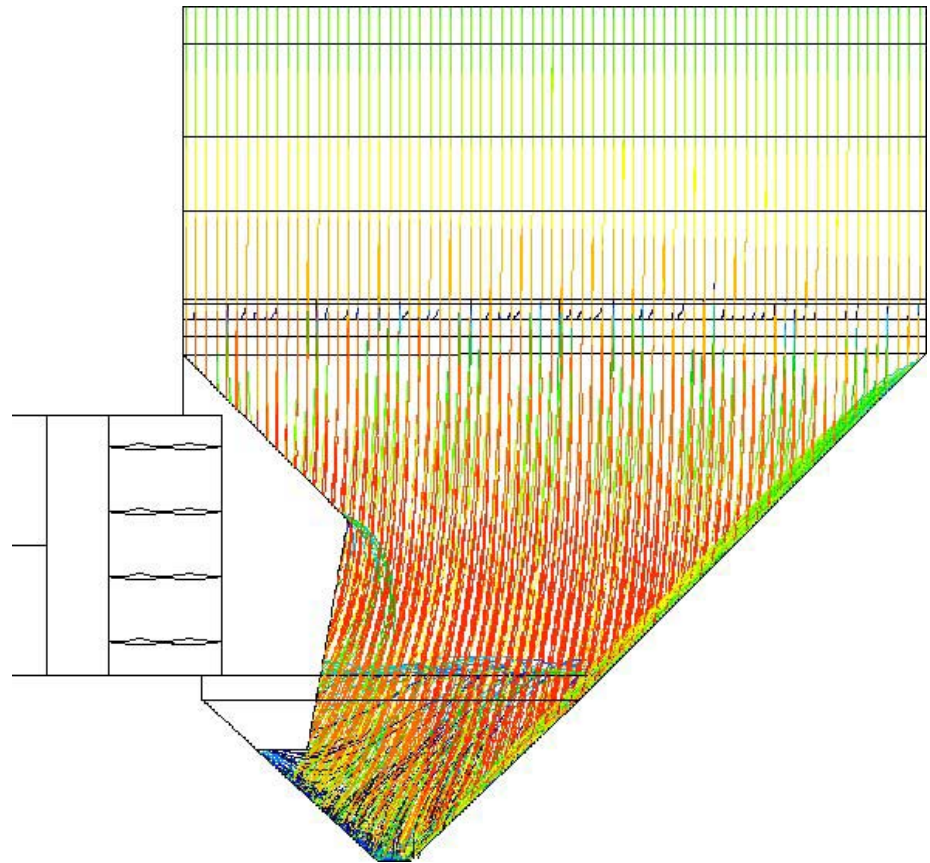
LPA Modeling via CFD

- ❖ Examine gas flow patterns and peak velocities through the system
- ❖ Track ash particles in flight through the ductwork and hopper regions
- ❖ Use model to evaluate wide range of design options



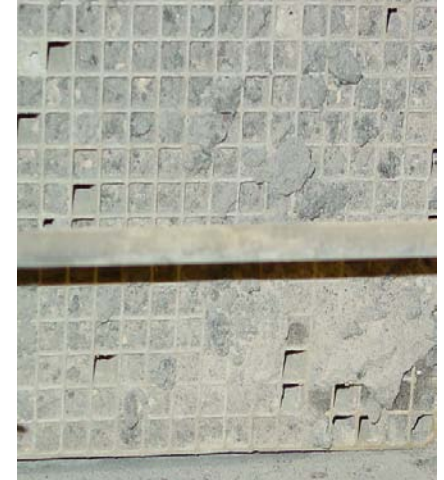
LPA Tracking in CFD

- ❖ Examine numerous particle sizes (3-7mm typical)
- ❖ Calculate particle paths
 - Rebound off surfaces
 - Impact on screen
 - Capture in hopper



SCR Large Particle Ash Capture

- ❖ Catalyst openings for coal-fired plants are smaller than LPA particles
- ❖ Once LPA becomes “wedged” into the catalyst, fine ash builds up as well
 - Hard to clean
 - Get dunes of ash on top layer catalyst



LPA System Design – Key Points

- ❖ Capture LPA in hoppers of adequate size
- ❖ LPA screens have become standard practice
- ❖ Ash deflection baffles also useful
- ❖ Screen erosion and pluggage remain issues



Model Accuracy

- ❖ Do physical and CFD models match field test data?
 - Field data is unfortunately limited
 - Tend to go by industry experience and whether catalyst performance goals are met
- ❖ Do CFD and physical models match each other?
 - For velocity and pressure drop predictions, correlation is quite good
 - For NH_3 injection correlation has improved steadily over time
 - Better CFD meshes (= mesh quality and level of detail)
 - Faster computers (= larger CFD meshes)
 - Models can even predict transient behavior

Flow Visualization

- ❖ Physical models – smoke flow, string tufts, dust injection/re-entrainment
- ❖ CFD models –animations of gas streamlines and particle pathlines

Conclusions – Flow Modeling

- ❖ CFD and physical modeling are applied to a wide range of equipment “from the fan to the stack”
- ❖ Modeling is an excellent tool for design optimization versus trial and error in the field
- ❖ There are a number of flow-related objectives when designing or optimizing equipment
- ❖ Often trade-offs exist, as objectives can be competing
- ❖ Accuracy of model results is quite good, as has comparison of results between model types, as long as proper attention is paid to mesh quality and laboratory test techniques

Ash Deposition

- ❖ Flues
- ❖ Turning vanes
- ❖ Catalyst



Ash Deposition – What Causes It?

- ❖ Low velocity regions
 - Due to non-uniform velocity distribution
 - Due to prolonged lower load operation
- ❖ Dead, recirculation zones
 - Sticky ash agglomerates, especially PRB and blends
 - Due to internal structure, flow separation, poor flow control
 - Due to flow angularity, causing local flow separation (particularly at catalyst inlet)
- ❖ Horizontal surfaces, beams, trusses
 - In SCR, can result in avalanche of accumulated ash, plugging catalyst
- ❖ Inleakage, moisture infiltration
- ❖ Sticky ash

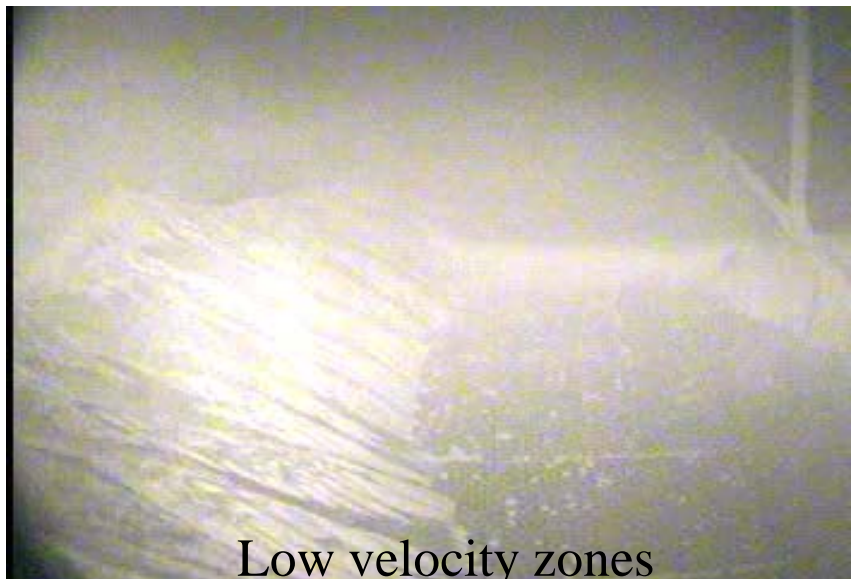
Ash Deposition – What Causes It?



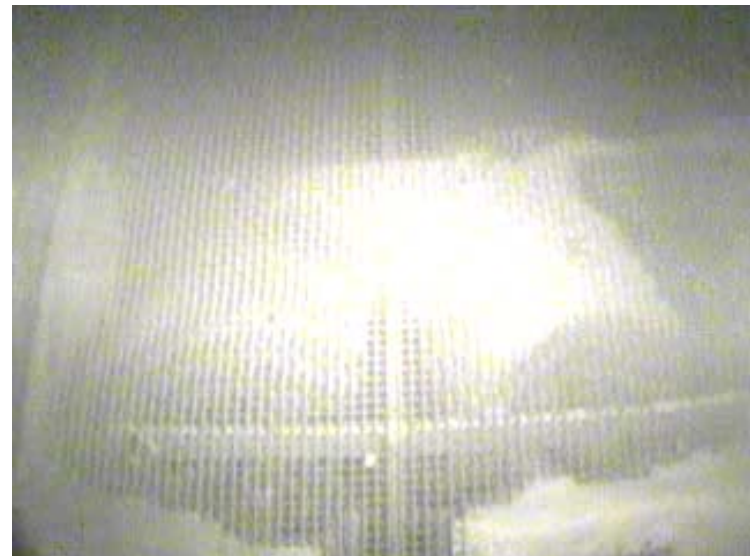
Accumulation on beams



Ash avalanche



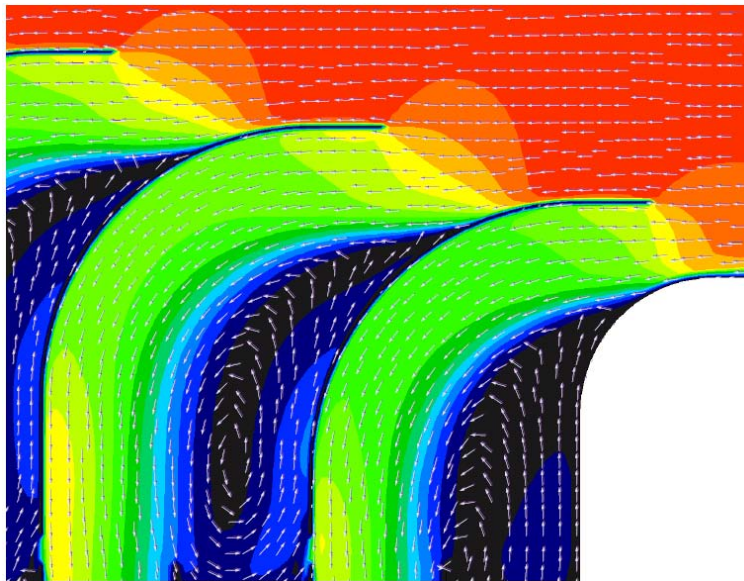
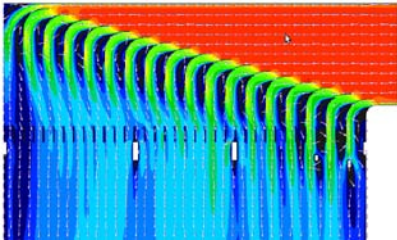
Low velocity zones



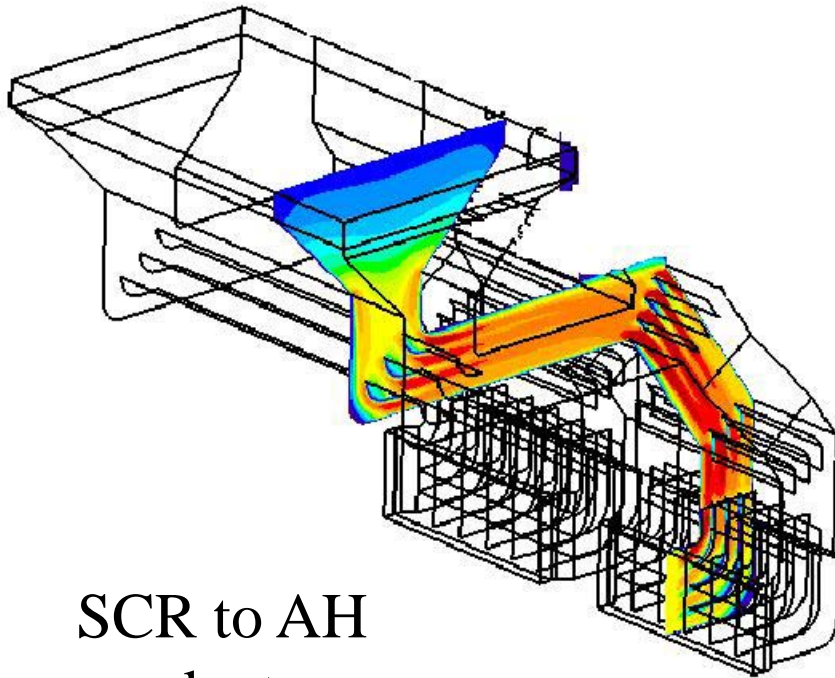
Ash Deposition – CFD Modeling

❖ CFD Model

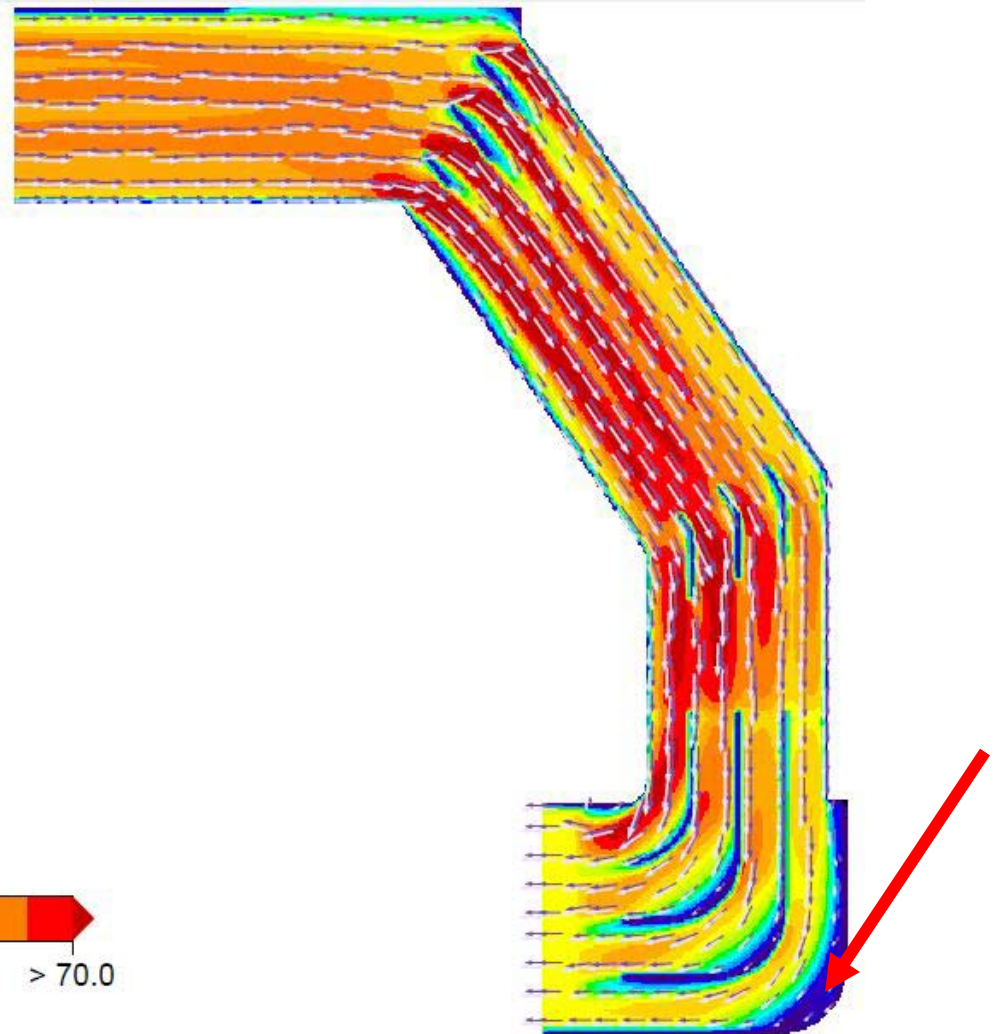
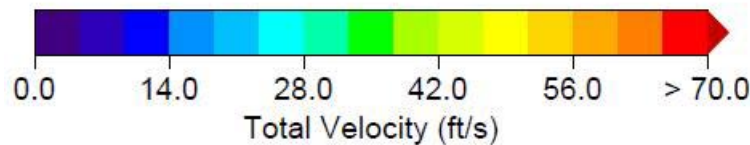
- Observe low velocity, recirculation flow zones
- Assess velocity patterns over the load range
- Can examine all locations throughout model (i.e., millions of data points)



Ash Deposition – CFD Modeling



SCR to AH
duct



Ash Deposition – CFD Modeling



A-side AH inlet

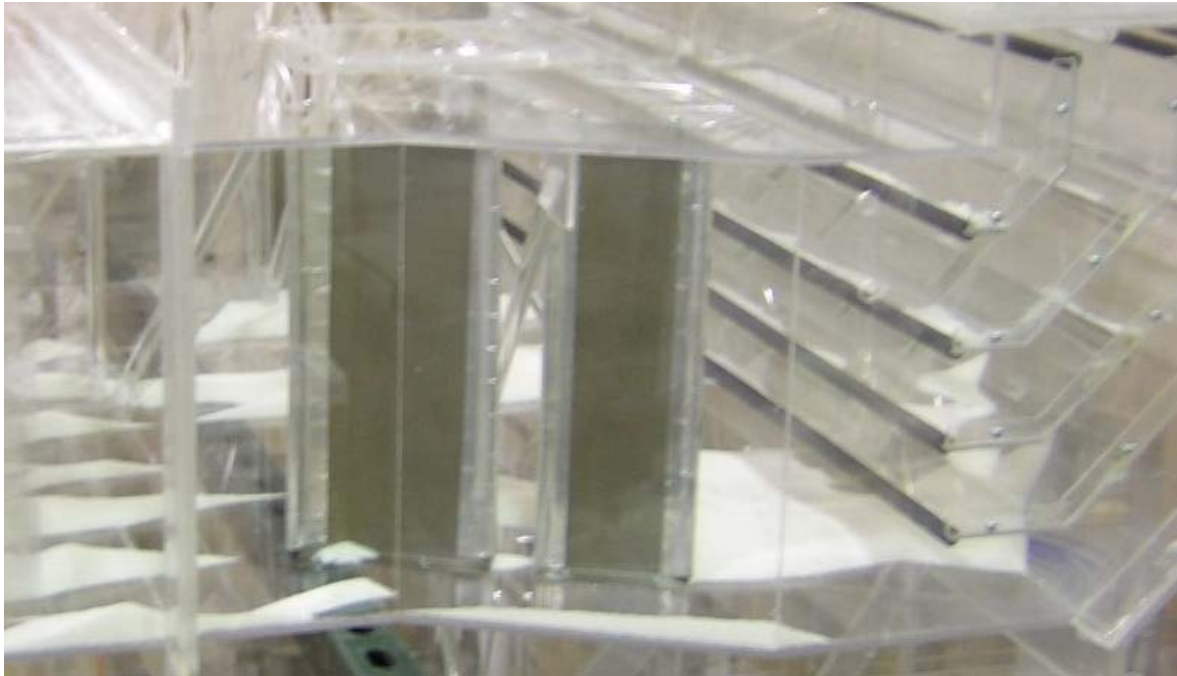


B-side AH inlet

Ash Deposition – Cold Flow Modeling

❖ Cold Flow Physical Model

- Perform “dust testing” to evaluate drop out and re-entrainment
- Use simulated ash (laboratory dust) under ambient conditions
- Match aerodynamics of dust to that of actual ash

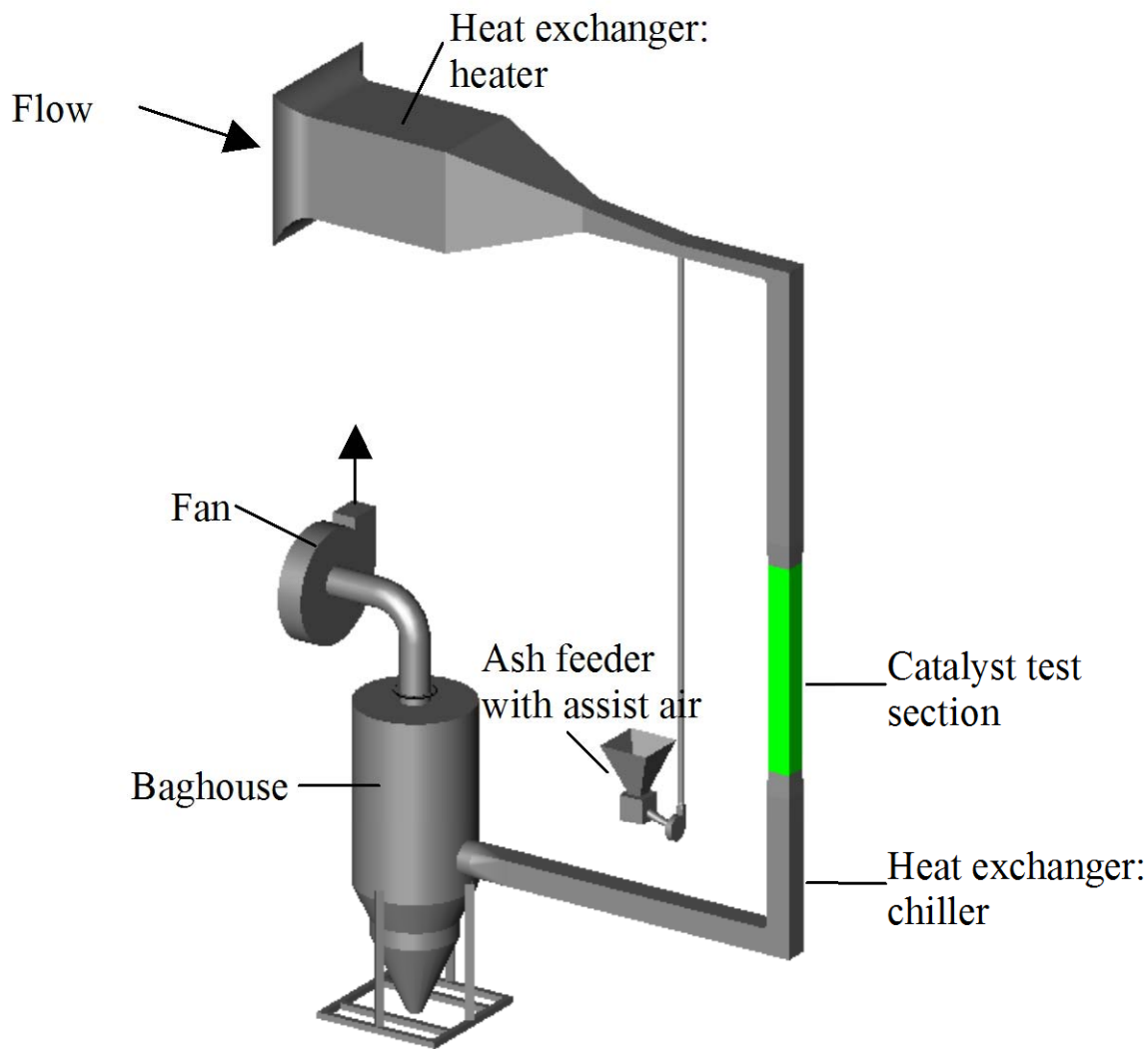


Ash Deposition – Hot Flow Modeling

❖ Hot Flow Model

- Testing under actual temperature conditions
- Real ash, not laboratory dust
- Downside is smaller scale, lack of flue gas constituents
- Recent research, not completed yet
- Flues and SCR pluggage

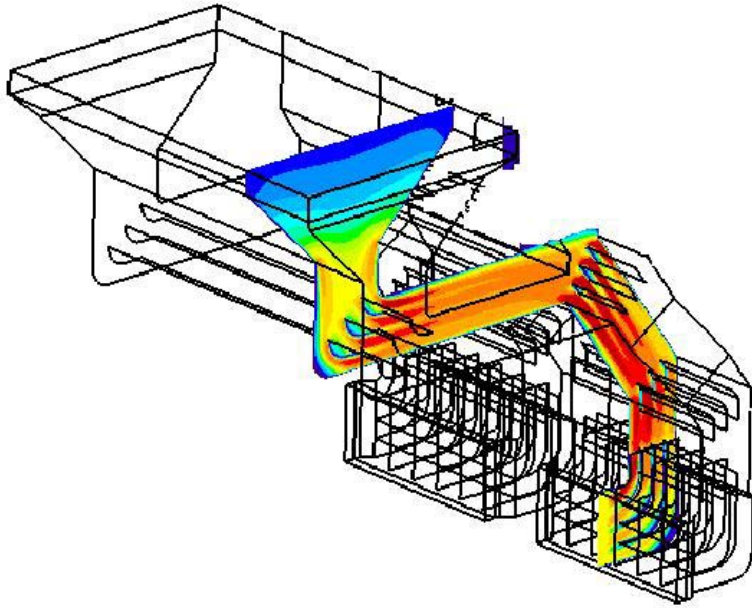
Ash Deposition – Hot Flow Modeling



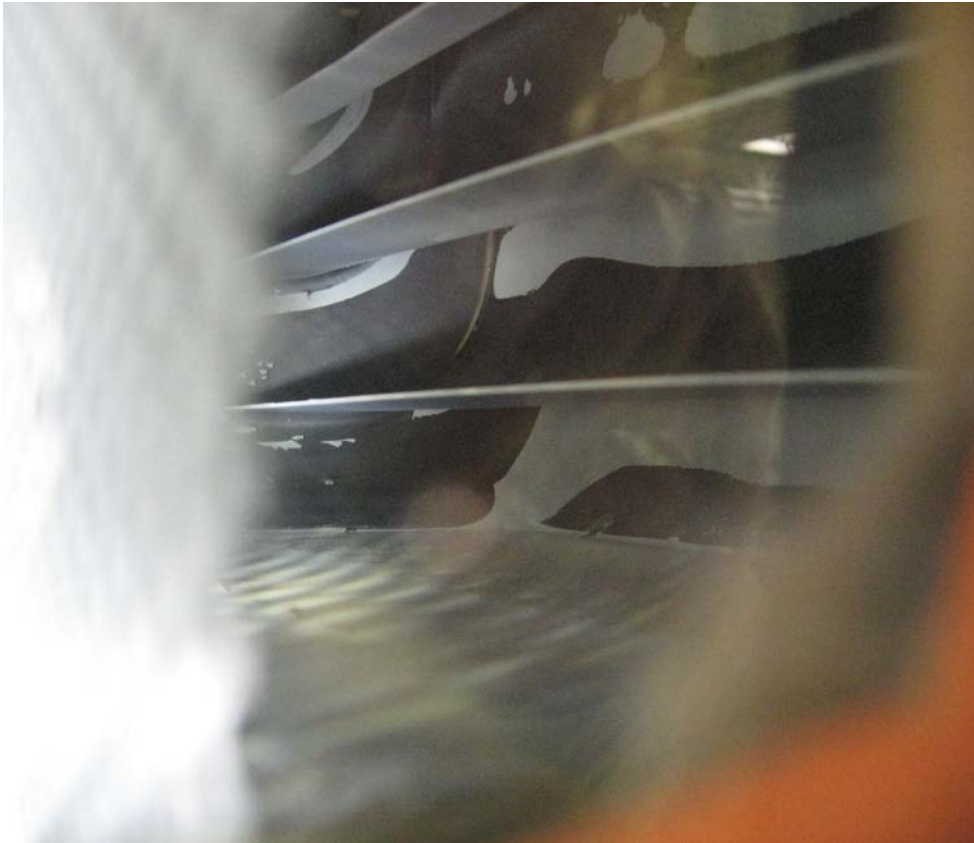
Ash Deposition – Hot Flow Modeling



Ash Deposition – Hot Flow Modeling



Ash Deposition – Hot Flow Modeling



Vanes in corner



Near AH

Conclusions – Ash Deposition

- ❖ Ash deposition and pluggage continue to be problems for plant equipment
- ❖ Modeling is used to minimize deposition potential
 - Standard modeling methods (CFD and cold flow modeling) are generally used
 - Hot flow modeling method is being evaluated
- ❖ Key elements to minimizing deposits include
 - Control and optimize velocity distribution (over the load range)
 - Avoid dead, recirculation zones
 - Minimize flow angularity / ash impingement angle at catalyst inlet
 - Address inleakage, moisture infiltration
 - Minimize horizontal surfaces / accumulation zones

Questions?